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(57) Abstract

Normally liquid, omega-hydrofluoroalkyl other compounds (and selected mixtures thereof) have a saturated perfluoroaliphatic chain of carbon atoms interrupted by one or more ether oxygen atoms. The compounds can be prepared, e.g., by decarboxylation of the corresponding fluoroalkyl ether carboxylic acids and are useful, e.g., in cleaning and drying applications.

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OMEGA-HYDROFLUOROALKYL ETHERS, PRECURSOR CARBOXYLIC ACIDS AND DERIVATIVES THEREOF, AND THEIR PREPARATION AND APPLICATION

This invention relates to omega-hydrofluoroalkyl ethers and their preparation and application. In another aspect, this invention relates to perfluoro-(alkoxyalkanoic) acids and derivatives thereof and their preparation. In another aspect, it relates to the preparation of perfluoro(alkoxyalkanoic) acids by direct fluorination of their hydrocarbon alkanoic acid or ester analogs and to the preparation of omega-hydrofluoroalkyl ethers, for example, by decarboxylation of said acids or their alkyl esters. In another aspect, this invention relates to uses of perfluoro(alkoxyalkanoic) acids and derivatives thereof.

Because of a steady flow of bad news about the damaged stratospheric ozone layer, the deadlines for the end to industrialized countries' production of chlorofluorocarbons ("CFCs") and other ozone-depleting chemicals were accelerated by countries who are parties to the Montreal Protocol on Substances That Deplete the Ozone Layer - see Zurer, P.S., "Looming Ban on Production of CFCs, Halons Spurs Switch to Substitutes," November 15, 1993, Chemical & Engineering News, p. 12.

Work is under way to replace CFCs and halons, such as CCl_2F_2 , CCl_3F , CF_3Br , and CCl_2FCClF_2 , with substitute or alternative compounds and technologies. A number of hydrofluorocarbons ("HFCs"), e.g., CH_2FCF_3 ("HFC-134a"), are being used or have been proposed as CFC substitutes (and HFC-134a has been characterized as being more "ozone friendly" - see U.S. Patent No. 5,118,494

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(Schultz et al.)). Hydrochlorofluorocarbons ("HCFCs"), such as CH_3CCl_2F ("HCFC-141b), as the <u>C&EN</u> article, supra, points out, are CFC substitutes, but although they are not nearly as damaging, these substitutes do carry ozone-depleting chlorine into the stratosphere. Another proposed substitute is the simple omegahydrodifluoromethyl perfluoromethyl ether, CF3OCF2H --See J.L Adcock et.al., "Fluorinated Ethers -- A new Family of Halons," 1991 CFC Conference Proceedings (1991). Another hydro-fluoroalkyl ether (or ether hydride), $F[CF(CF_3)CF_2O]_4CFHCF_3$, made by decarboxylation of the fluorinated 2-alkoxypropionic acid salt, has been tested as a blood emulsion -- see Chem. Pharm. Bull. 33, 1221 (1985).

U.S. Pat. No. 4,173,654 (Scherer) states that fluorocarbons due to their inertness have found use as electronic coolant or leak testing fluids, and other compounds having good solubility for oxygen have been investigated as artificial blood substitutes. patent describes certain fluorocarbon "hybrid" materials with metabolically active hydrocarbon moieties, such as, inter alia, -CH2-(CH2)m-H. U.S. Pat. No. 4,686,024 (Scherer et al.), which describes certain perfluorocyclic ethers, states that various perfluoro chemicals are disclosed in patents as being suitable as oxygen and carbon dioxide carriers. And International Application published as WO 93/11868 (Kaufman et al.) describes certain chlorofluorochemicals and emulsions thereof as useful in various oxygen transport applications, e.g., as oxygen transfer agents or 30 "artificial bloods."

There are a number of other patents describing various fluorocarbon ethers or polyethers. U.S. Patent No. 3,342,875 (Selman et al.) describes certain "hydrogen modified fluorocarbon ethers" (or "hydrogen capped polyethers") made, inter alia, by pyrolysis of a hydrogen-containing derivative of an ether, such as

the fluorocarbon ether acid or the ammonium salt, which ether is obtained by the polymerization of fluorocarbon epoxides. British Patent Specification 1,194,431 (Montecatini Edison S.P.A.) describes certain perfluorinated ethers and polyether derivatives having the general formula

$$CF_3 - O - (C_3F_5O)_M - (CF_2O)_N - (CF(CF_3) - O)_L - CF_2X$$

- where, <u>inter alia</u>, each subscript M, N, and L is zero or a whole number from 1 to 99, and X is a hydrogen atom or -COOMe wherein Me is an equivalent of an alkali or alkaline earth metal, an examples of which is pentafluorodimethyl ether, CF₃-O-CF₂H.
- U.S. Patent No. 3,597,359 (Smith) describes certain perfluoroalkylene ether-containing compound represented by the formula

$$R_{4}-R-O-(CF-CF-O)_{T1}$$
 $-(R_{5}-O)_{a}$ $(CF-CF-O)_{T1}$ $-(R_{5}-O)_{a}$ $(CF-CF-O)_{T2}$ $-(R_{5}-O)_{a}$ $(CF-CF-O)_{T3}$ $(CF-CF-O)_{T4}$ $(CF-CF-O)_{T5}$ $(CF-CF-O)_{$

- wherein, inter alia, R is alkylene, alkoxyalkylene, or perfluoroalkylene, R₁ is fluorine or trifluoromethyl provided not more than one R₁ is trifluoromethyl, R₂ is fluorine or trifluoromethyl provided not more than one R₂ is trifluoromethyl, R₃ is fluorine or trifluoromethyl, R₄ is hydrogen or halogen provided
- trifluoromethyl, R₄ is hydrogen or halogen provided that when R is alkylene or alkoxyalkylene R₄ is hydrogen, R₅ is perfluoroalkylene having at least 2 carbon atoms, R₆ is, inter alia hydrogen, trifluoromethyl or perfluoroethyl, a is zero or 1, n and m are whole numbers of 0 to 50, and n + m is 1 to 50.
 - U.S. Patent No. 3,962,460 (Croix et al.) describes aliphatic ethers, including those of the formulas

International Patent Application WO 90/01901 (Long)
describes certain perfluorocarbon hydrides, such as
perfluorocctyl hydride, used in emulsions for carrying
oxygen to the tissues of an animal body. European
Patent Application Publication No. 0 482 938 A1
(Chambers et al.) describes fluorinated ethers of the
formula

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wherein R is hydrogen, fluorine, or alkyl or fluoroalkyl of 1-6 carbon atoms, R' is hydrogen or alkyl or fluoroalkyl of 1 to 6 carbon atoms, and R" is fluorine or alkyl or fluoroalkyl of 1 to 6 carbon atoms.

Other patents describing one or more various fluoroalkoxyalkanoic acids and esters or other derivatives thereof and their preparation are U.S. Patent Nos. 2,713,593 (Brice et al.), 3,214,478 30 (Milian, Jr.), 3,393,228 (Braun), 4,118,421 (Martini), 4,357,282 (Anderson et al.), 4,729,856 (Bernonge), 4,847,427 (Nappa), 4,940,814 (Schwertfeger), 4,973,716 (Calini et al.), 5,053,536 (Bierschenk et al.) 5,093,432 (Bierschenk et al.), and 5,118,494 (Schultz 35 et al.) and PCT International Applications Pub. Nos. WO 90/03357 (Moore et al.) and WO 90/06296 (Costello et al.). The aforementioned Brice et al. patent describes fluorocarbons acids made by electrochemical fluorination including an acid having a boiling point 40 of 225°C and said to be $n-C_8F_{17}OC_2F_4CO_2H$. aforementioned Nappa, Bierschenk et al., Moore et al.,

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and Costello et al. publications describe the preparation of the fluorinated compounds by direct fluorination of hydrocarbon analog precursors.

In one aspect, this invention provides a normally liquid (i.e., liquid under ambient conditions of temperature and pressure) fluoroalkyl ether compound or a normally liquid composition consisting or consisting essentially of a selected mixture of such compounds, said compound having a saturated perfluoroaliphatic chain of carbon atoms (e.g., 4 to 30) interrupted by one or a plurality (e.g., 2 to 8) of ether (or catenary, i.e., in-chain) oxygen atoms. The chain carbon atom at one end (hereafter called the proximal end) of the chain is bonded to a hydrogen atom (i.e., an omega-hydro substituent, or primary hydrogen atom) and two fluorine atoms, said proximal carbon atom being the carbon atom of a difluoromethyl group or moiety, -CF2H, which is directly bonded to another chain carbon atom, such as that of perfluoroalkylene chain segment, $-C_NF_{2N}$, or to a said ether-oxygen. The carbon atom at the other end of the chain (the distal end) is part of a distal group selected from the group consisting of a difluoromethyl, a difluorochloromethyl, -CF2Cl, a perfluoroalkyl substituted with a saturated alicyclic moiety, e.g., c-C₆F₁₁-, a straight-chain perfluoroalkyl, and a branched chain perfluoroalkyl. In a said compound where said proximal end of the chain terminates in a difluoromethyl group bonded to an ether-oxygen atom, then said straight-chain perfluoroalkyl has at least 6 chain carbon atoms, e.g., 6 to 16 chain carbon atoms, and said branched-chain perfluoroalkyl has at least 4 carbon atoms, e.g., 4 to 16 carbon atoms. Examples of such omega-hydro fluoroalkyl ether compounds are:

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 $CF_3(CF_2)_4-0-CF_2CF_2H$ $CF_3(CF_2)_5-0-CF_2H$ $CF_3(CF_2)_7-0-(CF_2)_5H$ $CF_3(CF_2)_5-0-(CF_2)_2-0(CF_2)_2H$ $H(CF_2)_2-0-(CF_2)_2H$ $C1(CF_2)_4-0-(CF_2)_4H$

If a said "selected mixture," i.e., a predetermined mixture of selected omega-hydrofluoroalkyl ether compounds, is desired for a particular use, a said composition of this invention can be made consisting or consisting essentially of a mixture of two or more of said compounds each having a desired discrete, non-random molecular weight, the selected compounds preferably being those having complementary properties, e.g., for imparting improved stability to emulsions where they are incorporated as oxygen carriers in medical applications.

The term "perfluoro," such as in the case of "perfluoroaliphatic," "perfluoroalkylene," or "perfluoroalkyl," means that except as may be otherwise indicated there are no carbon-bonded hydrogen atoms replaceable with fluorine nor any unsaturation.

Omega-hydrofluoroalkyl ethers of this invention are hydrophobic and less oleophobic than the perfluoroalkyl ether analogs, chemically inert, thermally stable, water insoluble, and normally liquid (e.g., at 20°C), and they can be made in accordance with this invention in high yield, high purity, and with a wide range of molecular weights. The covalent bond between the omega-hydrogen and terminal carbon, i.e., the C-H bond, is generally degradable by atmospheric photo-oxidation, thus making the omega-hydrofluoroalkyl ethers environmentally acceptable or compatible. The omega-hydrofluoroalkyl ether compounds, or the normally liquid composition

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consisting or consisting essentially thereof, can be used in applications where the aforementioned CFCs, HCFCs or halons have been used, for example, as solvents for precision or metal cleaning of electronic articles such as disks or circuit boards, heat transfer agents, coolants in refrigerator or freezer compressors or air conditioners, blowing agents or cell size regulators in making polyurethane foam insulation, or chemical fire extinguishing agents in streaming applications, total flooding, explosion suppression and inertion, and as carrier solvents for highly fluorinated polyethers used as lubricants for magnetic recording media. Another field of utility for the omega-hydrofluoroalkyl ethers is in emulsions useful in various medical and oxygen transport applications, for example, artificial or synthetic bloods.

The above-described omega-hydrofluoroalkyl ethers of this invention can be prepared by decarboxylation of the corresponding precursor fluoroalkyl ether carboxylic acids and salts thereof or, preferably, the saponifiable alkyl esters thereof. Alternatively, the omega-hydrofluoroalkyl ethers can be prepared by reduction of the corresponding omega-chlorofluoroalkyl ethers (e.g., those described in WO 93/11868, supra). The perfluoroalkyl ether carboxylic acids (and esters) themselves -- some of which are believed novel compounds and they and their preparation are other aspects of this invention -- can be prepared by direct fluorination of their corresponding hydrocarbon analogs. The omega-hydrofluoroalkyl ethers are essentially pure fluorinated compounds and are useful as such or in the form of a normally liquid composition consisting or consisting essentially of a selected mixture of such compounds. The precursor perfluoroalkyl ether carboxylic acid and ester compounds, like the above-described omegahydrofluoroalkyl compounds of this invention, have a

saturated perfluoroaliphatic chain of a plurality of carbon atoms, said chain likewise being interrupted by one or a plurality of ether oxygen atoms, the proximal end of the chain being connected to a carboxyl group or alkyl ester thereof. This carboxyl group (or salts thereof or its saponifiable alkyl ester) can be decarboxylated, as mentioned above, and thereby replaced by the aforementioned omega-hydro substituent of the resulting omega-hydroalkyl ether of this invention.

The aforementioned novel perfluoroalkyl ether acids and esters can also be converted into various other derivatives, such as their ammonium salts, which have utility as surface active agents useful in modifying the surface tension or interfacial tension of liquids. These compounds are more soluble in aqueous media and other organic solvents than are the corresponding perfluoroalkanoic acid derivatives, and this enhances their utility as surface-active agents. The compounds can conveniently be prepared by direct fluorination of the corresponding hydrocarbon ether acids, or derivatives such as an ester, in high yields as single molecular species.

A class of the normally liquid, omega
hydrofluoroalkyl ether compounds of this invention can
be represented by the general formula:

$$X-R_{f}-O-(R_{f}'-O)_{n}-R_{f}''-H$$
 I

30 wherein:

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H is a primary hydrogen atom;

X is a fluorine atom, a primary hydrogen atom, or a primary chlorine atom bonded to a difluoromethylene (of $R_{\rm f}$);

n is a integer of 0 to 7, preferably 0 to 3;

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 R_f , R_f , and R_f " are the same or different perfluoroalkylene (linear or branched) groups, e.g., $-CF_2CF_2$ -, which are unsubstituted or substituted with a perfluoro organo group which can contain ether oxygen, for example, R_f can be $-CF_2CF(R_f)^* CF_2$ - or $-R_f$ " CF_2 - where R_f " is a saturated perfluoroalicyclic group having 4 to 6 ring carbon atoms, such as perfluorocyclohexyl or perfluorocyclohexylene;

with the proviso that when X is H or Cl, R_f has 1 to 18, preferably 2 to 18, chain carbon atoms, R_f ' has 1 to 12, preferably 2 to 12, chain carbon atoms, and R_f " has 2 to 12 chain carbon atoms; and with the further proviso that when X is F, then R_f has at least 4, preferably 4 to 18, chain carbon atoms, R_f ' has 1 or more, preferably 1 to 12, more preferably 2 to 12, chain carbon atoms, and R_f " has 2 or more, preferably 2 to 12, chain carbon atoms.

A subclass of polyether compounds within the scope of general formula I is represented by the general formula:

 $X-R_f-O-(CF_2CF_2-O)_m-R_f"-H$

II

where m is an integer of 0 to 7, and H, X, $R_{\bf f},$ and $R_{\bf f}"$ are as defined for formula I.

Another subclass of compounds within the scope of general formula I is represented by the general formula:

$$F-R_f-O-(R_f'-O)_p-R_f"-H$$
 III

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where p is an integer of 0 to 2 and H, $R_{\rm f}$, $R_{\rm f}$, and $R_{\rm f}$ " are as defined for formula I, except $R_{\rm f}$ has 4 to 12

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chain carbon atoms, $R_{\rm f}{}'$ has 1 to 12 chain carbon atoms, and $R_{\rm f}{}''$ has 2 to 12 chain carbon atoms.

Another class of the normally liquid, omegahydrofluoroalkyl ether compounds of the invention can be represented by the general formula:

$X-R_{f}-O(R_{f}'-O)_{n}R_{f}"-H$

10 wherein:

H is a primary hydrogen atom;

X is a fluorine atom, a primary hydrogen atom, or a primary chlorine atom;

n is an integer of 0 to 7; and

R_f, R_f', and R_f" are independently selected from the group consisting of linear or branched, unsubstituted perfluoroalkylene groups; linear or branched, perfluoroalkyl- or perfluorocycloalkyl-substituted

perfluoroalkylene groups; and linear or branched perfluoroalkylene groups substituted with an ether oxygen-containing moiety;

with the proviso that when X is H or Cl, R_f has 1 to 18 chain carbon atoms and each of R_f ' and R_f " independently has 1 to 12 chain carbon atoms;

and with the further proviso that when X is F, then R_f has at least 4 chain carbon atoms and each of $R_f{}^\prime$ and $R_f{}^{\prime\prime}$ independently has 1 or more chain carbon atoms;

and with the still further proviso that when n is zero, then R_f is a perfluorocycloalkyl-substituted perfluoroalkylene group.

A list of representative examples of the omegahydrofluoroalkyl ether compounds of this invention is as follows.

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Table A

	1.	$CF_3(CF_2)_5-O-CF_2H$
	2.	$CF_3(CF_2)_3-O-(CF_2)_2H$
	3.	$c-C_6F_{11}CF_2-O-(CF_2)_2H$
5	4.	$CF_3(CF_2)_3$ -O- $CF_2C(CF_3)_2CF_2H$
	5.	(CF ₃) ₂ CFCF ₂ -O-CF ₂ H
	6.	$CF_3(CF_2)_4-0-(CF_2)_5H$
	7.	$CF_3(CF_2)_6$ -O- CF_2H
	8.	$CF_3(CF_2)_5-0-(CF_2)_2H$
10	9.	$CF_3(CF_2)_5-0-(CF_2)_3H$
	10.	$CF_3(CF_2)_6-0-(CF_2)_2H$
	11.	$CF_3(CF_2)_7$ -O- CF_2H
	12.	$CF_3(CF_2)_7 - O - (CF_2)_5 H$
	13.	$CF_3(CF_2)_7 - O - (CF_2)_6 H$
15	14.	$CF_3(CF_2)_5-O-(CF_2)_2-O-CF_2H$
	15.	$CF_3(CF_2)_5-0-(CF_2)_2-0-(CF_2)_2H$
	16.	$H-(CF_2)_2-O-(CF_2)_2H$
	17.	$H-(CF_2)_4-O-(CF_2)_4H$
	18.	$H-(CF_2)_2-O-(CF_2)_2-O-(CF_2)_2H$
20	19.	$H-CF_2-O-CF_2C(CF_3)_2CF_2-O-CF_2H$
	20.	$Cl(CF_2)_4-O-(CF_2)_4H$
	21.	$H(CF_2)_2OCF_2C(CF_3)_2CF_2O(CF_2)_2H$
	22.	C ₈ F ₁₇ OCF ₂ OC ₃ F ₆ H
	23.	$(CF_3)_3COC_2F_4OCF_2OC_2F_4OCF_2H$
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As mentioned above, the omega-hydrofluoroalkyl ether compounds or compositions of this invention can be made by decarboxylation of their corresponding precursor perfluoroalkyl ether carboxylic acids, hydrolyzable carboxylic acid derivatives, or 30 . hydrolyzable precursors thereto (some of which are believed novel). A class of such precursor compounds can be represented by the general formula:

$$R_{fp} = O(R_f'O)_n R_f'' = Z'$$
 IV

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wherein

R_{fp} is ROC(O)R_f or F-R_f, R_f being a
 perfluoroalkylene group as defined for
 formula I;

 R_{f}' and R_{f}'' are also perfluoroalkylene groups as defined for formula I;

n is also as defined for formula I; and Z' is a $\mathrm{CO_2H}$, $\mathrm{CO_2R}$, COF , COCl , $\mathrm{CONR^1R^2}$, or $-\mathrm{CF_2OC}(0)\mathrm{R_f}$, where R is selected from the group consisting of hydrogen, alkyl (such as a lower alkyl group of 1 to 6 carbon atoms), cycloalkyl, fluoroalkyl, and aryl, and where $\mathrm{R^1}$ and $\mathrm{R^2}$ are independently selected from the group consisting of hydrogen, alkyl, cycloalkyl, and heteroatom-containing cycloalkyl.

In the decarboxylation of the compounds of formula IV, the moiety Z' is replaced by a hydrogen atom.

Subclasses of said ether acids and derivatives thereof, which have other utilities in addition to their use as precursors of the omega-hydro ether compounds of this invention, for example, as surface active agents (or surfactants), as mentioned above, and which are believed novel, can be represented by the general formulas V, VI, VII, VIII and IX below,

R_{fo} -O- R_{fo} '-Z V

30 wherein:

R_{fo} is a perfluoroalkyl group (linear or branched).

having, for example, 1 to 18 carbon atoms,

preferably 1 to 12 carbon atoms,

 R_{fo}' is a perfluoroalkylene group (linear or branched) having, for example, 2 to 11 carbon atoms, at least one of R_{fo} and R_{fo}' having at least 8 chain carbon atoms; and

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z is -cooh, -coom_{1/v}, -coonh₄, -coor, -ch₂oh, -cof, -cocl, -cr, -conr, -ch₂nh₂, -ch₂nco, -cn, -ch₂oso₂r, -ch₂ocor, -ch₂ococr=ch₂, -conh(ch₂)_msi(or)₃, or -ch₂o(ch₂)_msi(or)₃, where M is an ammonium radical or a metal atom having a valence "v" of 1 to 4, such as Na, K, Ti, or Al, and each R is independently an alkyl (e.g., with 1 to 14 carbon atoms) or cycloalkyl, which groups can be partially or fully fluorinated, or an aryl (e.g., with 6 to 10 ring-carbon atoms), any of which groups can contain heteroatom(s), and m is an integer of 1 to about 11.

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wherein:

 R_{fq} (O-CF₂CF₂) a OCF₂-Z VI

R_{fq} is a perfluoroalkyl group (linear or branched) having from about 6 to about 18 carbon atoms, preferably 6 to 12 carbon atoms,

subscript a is an integer of at least 2, preferably 3 to 7, but when a is 2, then R_{fq} has at least about 8 carbon atoms; and Z is as defined for formula V.

 $R_{fr}-O-CF_2-O-R_{fr}'-Z \qquad VII$

wherein:

R_{fr} is a perfluoroalkyl group (linear or branched) having, for example, 2 to 18 carbon atoms, preferably 4 to 12 carbon atoms;

R_{fr}' is a perfluoroalkylene group (linear or branched) having, for example, 1 to 11 carbon atoms and preferably 1 to 5 carbon atoms; and

Z is as defined for formula V; and the sum of the number of carbon atoms in the groups $R_{\rm fr}$ and $R_{\rm fr}$ ' is at least about 7.

R_{fs}-O(CF₂)_b-Z VIII

wherein:

R_{fs} is a perfluoroalkyl group (linear or branched) having, for example, 1 to 18 carbon atoms, preferably 1 to 12 carbon atoms;

b is an integer of at least 3, preferably 3 to 11;

Z is as defined for formula V.

 R_{ft} -(O- R_{ft} ')_c-O-(CF₂)_d-Z IX

10 wherein:

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R_{ft} is a perfluoroalkyl group (linear or branched) having, for example, 1 to 18 carbon atoms, preferably 1 to 12 carbon atoms;

R_{ft}' is a perfluoroalkylene group (linear or branched) having, for example, 1 to 11 carbon atoms, preferably 2 to 4 carbon atoms;

c is an integer of at least 1, preferably 1 to 4;

d is an integer of 3 or greater, preferably 3 to 9; and

Z is as defined for formula V.

The carboxylic acids of formulas V to IX are useful intermediates for the preparation of many of the other derivatives of formulas V to IX. These derivatives include nonfunctional or functional 25 derivatives such as, for example, carboxylic acids, salts, esters, amides, nitriles, alcohols, acrylates, and vinyl ethers. Various patents describe processes for the preparation of a host of functional derivatives of oxyperfluoroalkylene compounds, i.e., 30 . perfluoropolyethers, e.g., see U.S. Pat. Nos. 3,250,808 (Mitsch et al.) and 4,094,911 (Moore et al.). derivatives have utility for various applications, such as surfactants, elastomers, coatings, lubricants, substances used in the preparation of liquid crystal 35 materials such as those in U.S. 5,262,082 (Janulis et al.), and in the treatment of fibrous substrates to

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impart oil and water repellency thereto. The ammonium salts of the carboxylic acid derivatives are particularly useful as surfactants.

The carboxylic acid compounds of formula V are normally solid. The carboxylic acid compounds of formulas VI, VII, VIII and IX generally are normally liquid and normally liquid compositions can be made up which consist or consist essentially of selected mixtures of such compounds.

A list of representative examples of fluoroalkylether acids (or derivatives) which can be utilized to prepare omega-hydrofluoroalkyl ethers of this invention is as follows:

Table B

1.	CF3(CF2))7-0-CF2C02H
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2.
$$CF_3(CF_2)_{11}-O-CF_2CO_2H$$

3.
$$CF_3(CF_2)_6-O-C_2F_4CO_2H$$

4.
$$CF_3(CF_2)_4-0-C_2F_4CO_2H$$

5.
$$CF_3(CF_2)_5-O-C_2F_4CO_2H$$

6.
$$CF_3(CF_2)_8-O-C_2F_4CO_2H$$

7.
$$CF_3(CF_2)_7-0-C_2F_4CO_2H$$

8.
$$CF_3(CF_2)_9 - O - C_2F_4CO_2H$$

9.
$$CF_3(CF_2)_{11}-O-C_2F_4CO_2H$$

10.
$$CF_3(CF_2)_5 - OC_2F_4O - C_2F_4CO_2H$$

11.
$$C_8F_{17}-O-(CF_2)_5CO_2H$$

12.
$$C_{10}F_{21}-0-(CF_2)_5CO_2H$$

13.
$$CF_3-O-(CF_2)_7CO_2H$$

14.
$$C_2F_5-0-(CF_2)_7CO_2H$$

15.
$$C_3F_7-O-(CF_2)_7CO_2H$$

16.
$$CF_3-O-(CF_2)_9CO_2H$$

17.
$$CF_3-O-(CF_2)_{10}CO_2H$$

18.
$$CF_3(CF_2)_5 - O - C_2F_4 - O - C_2F_4 - O - C_2F_4 - O$$

19.
$$CF_3(CF_2)_7 - O + C_2F_4 - O - C_2F_4$$

•	20.	$CF_3(CF_2)_9 - O - C_2F_4 - O$
	CF ₂ C	O ₂ H
	21.	$CF_3(CF_2)_{11}-O-C_2F_4-O-C_2F_5-C$
	CF ₂ C	o ₂ H
5	22.	$CF_3(CF_2)_{11} - (OC_2F_4)_{1-5} - O - CF_2CO_2H$ from
		Brij tm 30 acetate
	23.	$C_6F_{13}OCF_2O(CF_2)_5CO_2H$
	24.	$CF_3(CF_2)_7 - O - CF_2 - O - CF_2CO_2H$
	25.	$CF_3(CF_2)_7-0-CF_2-0-C_3F_6C0_2H$
10	26.	$(CF_3)_3COC_2F_4OCF_2OC_2F_4CO_2H$
	27.	$C_4F_9-O-(CF_2)_3CO_2H$
	28.	C_5F_{11} -O-(CF ₂) ₃ CO ₂ H
	29.	C ₆ F ₁₃ -O-(CF ₂) ₃ CO ₂ H
	30.	C ₅ F ₁₁ -O-(CF ₂) ₄ CO ₂ H
15	31.	$CF_3 - O - (CF_2)_5 CO_2 H$
	32.	C ₄ F ₉ -O-(CF ₂) ₅ CO ₂ H
•	33.	C ₅ F ₁₁ -O-(CF ₂) ₅ CO ₂ H
	34.	$C_4F_9-O-C_4F_8-O(CF_2)_3CO_2H$
	35.	$C_6F_{13}-O-C_4F_8-O(CF_2)_3CO_2H$
20	36.	C ₄ F ₉ -O-C ₂ F ₄ O-C ₂ F ₄ O(CF ₂) ₃ CO ₂ H
	37.	$CF_3-O-(C_2F_4O)_3-(CF_2)_3CO_2H$
	38.	C ₈ F ₁₇ OCF ₂ OC ₅ F ₁₀ CO ₂ H
	39.	$(CF_3)_3COC_2F_4OCF_2OC_2F_4OCF_2CO_2H$
		(CF ₃) ₂ CFCF ₂ CF ₂ O(CF ₂) ₅ CO ₂ H
25		CF ₃ (CF ₂) ₇ OC ₂ F ₄ OC ₂ F ₄ OCF ₂ CO ₂ H
	42.	CF ₃ (CF ₂) ₁₁ OC ₂ F ₄ OC ₂ F ₄ OCF ₂ CO ₂ H
	•	31 2131 2 4 2 4 2 2

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The following presents overall schemes of reactions that can be used in the preparation of omega-hydrofluoroalkyl ethers of this invention using general formulas defined above. In these schemes, the illustrated reaction results in the product whose formula is depicted on the succeeding line

Scheme I

a.
$$R \longrightarrow (R' \longrightarrow R'' - C(0)) OR$$
 $\xrightarrow{F_2}$ direct fluorination

c.
$$Rf - O - (Rf - O)_n Rf'' - C = O O O (H \text{ or } CH_3) \frac{KOH + \Delta}{\text{decarboxylation}}$$

$$R_f \!\!-\!\! O \!\! \left[\!\! - \!\! R_f \!\!\! - \!\!\! O \!\! \right]_{\!\! \, \underline{n}} R_f \!\!\! '' - \!\!\! H$$

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Scheme II

a. $R=0-(R'-0)_{n}R''-CH_{2}=0-COCH_{3}$ F₂ direct fluorination

c.
$$R_{f}=0-(R_{f}'-0)_{n}R_{f}''-CO=0$$
 (H or CH_{3}) KOH + Δ

Scheme III

a.
$$R = O - (R' - O)_n - R'' - Cl$$
 $\frac{F_2}{\text{direct fluorination}}$

b.
$$R_f - O - \left(R_f' - O\right)_n - R_f'' - C1$$
 Raney Ni

The ether alpha and omega dihydrides, that is, where X in formula I is H, may be prepared by analogous schemes. For example, the following Scheme IV is analogous to Scheme I

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Scheme IV

- a. CH;0-CO-R-O (R'-O) -R"-CO-OCH; direct fluorination
- b. CF20-CO-Rf-0-Rf'-0)n-Rf"-CO-OCF; hydrolysis or methanolysis
- c. (H or CH₃) OCOR fO(Rf'=0) Rf"=CO=O(H or CH₃) KOH + A decarboxylation

Looking first at Scheme I above, in the direct fluorination, step "a", a fluorinatable precursor ether carboxylic acid ester, e.g., C4H9-O-(CH2)5COOCH3, is directly fluorinated by contact with fluorine gas. (The term "fluorinatable" means that the precursor contains carbon-bonded hydrogen atoms which are replaceable with fluorine and the precursor may contain unsaturation which can be saturated with fluorine.) The resulting fluorinated ether acid ester compound, depicted in step b, can be made with essentially the same number and spatial arrangement of carbon and oxygen atoms as the precursor thereof. fluorinated ether acid composition which consists or consists essentially of a selected mixture of fluorinated ether compounds is desired, a selected mixture of the corresponding precursor compounds can be fluorinated or, alternatively, the selected precursor compounds can be separately fluorinated and then blended.

The direct fluorination of the fluorinatable ether precursor can be carried out at temperatures typically used in direct fluorination, e.g., at moderate or near ambient temperatures such as -20°C to +50°C, using a stoichiometric excess of fluorine gas, which is preferably diluted with an inert gas, such as nitrogen,

to minimize or avoid the hazards of pure fluorine gas and to control the amount of heat generated upon contact of the precursor with fluorine. fluorination is preferably carried out in an oxygenand water-free environment and can be carried out in the presence of solid, particulate scavenger, e.g., sodium fluoride, for the hydrogen fluoride by-product generated. Liquid phase direct fluorination can be employed and involves using an inert liquid, such as a fluorocarbon or chlorofluorocarbon liquid, as a Both scavenger and an inert liquid reaction medium. reaction medium can be utilized, if desired. fluorination is preferably carried out by liquid phase direct fluorination in the absence of hydrogen fluoride scavenger by using a temperature and inert gas flow rate sufficient to volatilize hydrogen fluoride byproduct and enable its removal from the fluorination zone as it is generated.

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In another aspect, this invention provides a fluorochemical composition containing the fluorinated ether acid or derivative thereof, hereinbefore described, as the sole essential component of the fluorochemical composition.

Although direct fluorination is a substitution method involving the replacement of hydrogen atoms with fluorine, direct fluorination provides higher yields and purer products than do other substitution methods such as the electrochemical fluorination and cobalt trifluoride methods -- see, for example, U.S. Pat. No. 5,093,432 (Bierschenk et al.). The purity of the perfluorinated ether acid (or ester) compositions of the invention is further enhanced by the use of single precursor compounds or selected (rather than random) mixtures thereof.

The preferred method of fluorination is the "liquid phase direct fluorination technique," which involves making a very dilute dispersion or,

preferably, solution of the precursor(s) in a liquid reaction media, which is relatively inert to fluorine at the fluorination temperatures used, the concentration of fluorinatable starting material thus being relatively low so as to more easily control the 5 reaction temperature. The reaction mixture can also contain or have dispersed therein a hydrogen fluoride scavenger such as sodium fluoride, the scavenger: precursor weight ratio being, for example, from about 0.5:1 to 7:1. The reaction mixture can be 10 vigorously agitated while the fluorine gas is bubbled through it, the fluorine preferably being used in admixture with an inert gas, such as nitrogen, at a concentration of about 5 to 50 volume %, more preferably about 10 to 25 volume %, and being 15 maintained in stoichiometric excess throughout the fluorination, e.g., up to 15 to 40%, or higher, depending on the particular starting material and the efficiency of the equipment used, such as the reactor 20 agitation. Yields generally in the range of about 30-77 mole %, and, with experience, as high as 65 to about 85 mole %, of the perfluorinated product may be achieved by this method.

Suitable liquids useful as reaction media for the liquid phase direct fluorination technique are 25 chlorofluorocarbons such as Freon™ 11 fluorotrichloromethane; chlorofluoroethers; Fluorinertm electronic liquids FC-75, FC-72, and FC-40; perfluoroalkanes such as perfluoropentane and 30 perfluorodecalin; perfluoropolyethers; and perfluoroacetals. Mixtures of such liquids can be used, e.g., to get good dispersion of precursor and intermediate reaction products. The reaction media are conveniently used at atmospheric pressure. Lower 35 molecular weight members of the above classes of reaction media can also be used, but elevated pressures are then required to provide a liquid phase.

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The liquid phase direct fluorination reaction is generally carried out at a temperature between about -10°C to +50°C, preferably between about -10°C to 0°C if a hydrogen fluoride scavenger is used, and, if such a scavenger is not used, between about 0°C to 150°C, preferably about 0°C to 50°C, most preferably about 10°C to 30°C, the temperature being sufficient to volatilize the hydrogen fluoride by-product and, with the aid of the inert gas, flowing at a sufficient rate, cause the purging of the by-product from the fluorination reactor as it is generated. At these temperatures, the liquids utilized as reaction media do not react appreciably with the diluted fluorine and are essentially inert. The reaction medium and other organic substances may to some extent be present in the gaseous reactor effluent, and a condenser may be used to condense the gaseous reaction medium and such substances in the effluent and permit the condensate to return to the reactor. The condenser can be operated so as to minimize or prevent the return to the reactor of hydrogen fluoride by-product (which could have an adverse effect on yield of product if allowed to remain in the reactor during fluorination). The return of the hydrogen fluoride can be minimized or prevented by selective condensation of the organic materials while allowing the hydrogen fluoride to pass through the condenser, or by total condensation of both hydrogen fluoride and the organic materials into a separate vessel and followed, if desired, by separation of the hydrogen fluoride as the upper liquid phase and the return of the lower liquid phase.

The liquid phase fluorination reaction may be carried out in a batch mode, in which all of the precursor is added to the liquid prior to fluorination to provide a precursor concentration of up to about 10% by weight, and the fluorine-containing gas is then bubbled through the precursor-containing liquid. The

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reaction can also be carried out in a semi-continuous mode, in which the precursor is continuously pumped or otherwise fed neat, or as a diluted solution or dispersion, in a suitable liquid of the type used as a reaction medium, into the reactor, e.g., at a rate of about 1 to 3 g/hr into 400 mL of liquid reaction mixture, as fluorine is bubbled through, e.g., at a fluorine flow rate of about 40 to 120 mL/min and an inert gas flow rate of about 150 to 600 mL/min. fluorination can also be carried out in a continuous manner, in which the precursor (either neat or dissolved or dispersed in a suitable liquid of the type used as a reaction medium) is continuously pumped or otherwise fed into the reactor containing the reaction medium as the fluorine-containing gas is introduced, as described above, and the stream of unreacted fluorine, hydrogen fluoride gas, and inert carrier gas is continuously removed from the reactor, as is a stream of liquid comprising perfluorinated product, incompletely fluorinated precursor, and inert liquid reaction medium, and the necessary separations are made to recover the fluoroalkyl ether composition. desired, the unreacted fluorine and the incompletely fluorinated precursor can be recycled. The amount of inert liquid medium in the reactor can be maintained at a constant level by addition of recycled or fresh liquid.

Due to the extremely high exothermicity of the fluorination reaction, a cooled liquid or ice bath is generally employed in order that acceptable rates of reaction may be achieved. When the reaction is complete, the reactor is purged of fluorine and the reactor contents are removed. Where the fluorination is carried out by the liquid phase fluorination technique in the presence of a hydrogen fluoride scavenger, the spent scavenger can be separated by filtration or decantation from the liquid reactor

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contents and the latter then distilled to separate the reaction medium from the crude product. Where the fluorination is carried out by the liquid phase fluorination technique without using the scavenger, the reaction product mixture can be distilled to recover the product.

Useful representative precursor fluorinatable ether acid esters which can be used to prepare the omega-hydrofluoroalkyl ethers of this invention are the hydrocarbon counterparts of the structures listed in Table A above, except that instead of the terminal hydrogen atom the structures of the esters terminate with -2' (where Z' is as defined for formula IV) or -CH₂OC(O)R (as shown in Scheme II <u>supra</u>) and that the precursors can contain unsaturation.

Representative examples of the fluoroether acids of or used in this invention include the perfluorinated (i.e., having essentially all hydrogens replaced with fluorine) counterparts of the precursor fluorinatable acid esters described above. When the precursors have unsaturation, the corresponding fluorinated ether acids are saturated.

As pointed out above, the fluoroether acids and derivatives can be used as precursors in the preparation of the omega-hydrofluoroalkyl ethers and they are also useful, for example, as surfactants.

The above-described fluoroether acids or the esters thereof, e.g., alkyl esters such as the methyl ester, can be converted by a decarboxylation process to the omega-hydrofluoroalkyl ethers of this invention. In one such process, a solution of KOH in ethylene glycol is prepared and the fluoroether acid or ester precursor is added thereto (neat or as a solution in an inert solvent liquid such as a perfluorinated liquid), preferably dropwise with stirring at ambient or room temperature. The resulting mixture can then be heated slowly, for example, to 190°C, during which time the

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methanol (from the saponification of a methyl ester), water (from neutralization of an acid), and decarboxylated product are distilled. The omegahydrofluoroalkyl ethers of the invention are surprisingly stable under such harsh basic conditions. An inert solvent liquid, if used, can be removed, for example, at low temperature under vacuum after neutralization. The resulting distillate, comprising the omega-hydrofluoroalkyl ether product, can be washed with water, dried with silica gel or magnesium sulfate, and then distilled to purify the product. If desired, the hydrofluoroalkyl ether product can be refluxed with a solution of potassium permanganate in acetone to remove easily-oxidized impurities. The yields of the ether product are generally high and the product generally will be quite pure and consist or consist essentially of the desired omega-hydrofluoroalkyl ether.

The omega-hydrofluoroalkyl ether compositions are non-toxic and capable of dissolving and transporting 20 oxygen and are therefore potentially useful as blood substitutes which can be employed invasively in the treatment of trauma, vascular obstructions, as adjuvants to cancer radiation treatment or chemotherapy, and as imaging contrast agents. For such 25 uses, emulsions of the compositions can be prepared by methods such as those described, for example, in U.S. Pat. Nos. 3,911,138 (Clark) and 5,077,036 (Long) and the PCT International Application published as WO 93/11868 (Kaufman et al.). The omega-hydrofluoroalkyl 30 . ether compositions are also useful as solvents for cleaning and drying applications such as those described in U.S. Patent Nos. 5,125,089 (Flynn et al.), 3,903,012 (Brandreth), and 4,169,807 (Zuber). Minor amounts of optional components, e.g., surfactants, may 35 be added to the fluoroether compositions to impart particular desired properties for particular uses. The

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ether compositions are also useful as heat transfer agents or coolants in refrigerator or freezer compressors or air conditioners, blowing agents or cell size regulators in making polyurethane foam insulation, or chemical fire extinguishing agents in streaming applications, total flooding, explosion suppression and inertion, and as carrier solvents for highly fluorinated polyethers used as lubricants for magnetic recording media.

In using the omega-hydrofluoroalkyl ether compositions of this invention for the drying of or displacing water from the surface of articles, such as circuit boards, the processes of drying or water displacement described in U.S. Patent No. 5,125,978 (Flynn et al.) can be used. Broadly, such process comprises contacting the surface of an article with a liquid composition comprising the ether composition of this invention, preferably in admixture with a nonionic fluoroaliphatic surface active agent. The wet article is immersed in the liquid composition and agitated therein, the displaced water is separated from the liquid composition, and the resulting water-free article is removed from the liquid composition. Further description of the process and the articles which can be treated are found in said U.S. Patent No. 5,125,978.

In using the ether composition of this invention as a heat transfer liquid in vapor phase soldering, the process described in U.S. Patent No. 5,104,034 (Hansen) can be used. Briefly, such process comprises immersing the component to be soldered in a body of vapor comprising the ether composition of this invention to melt the solder. In carrying out such a process, a liquid pool of the ether composition of this invention can be heated to boiling in a tank to form a saturated vapor in the space between the boiling liquid and a condensing means, a workpiece to be soldered is

immersed in the vapor whereby the vapor is condensed on the surface of the workpiece so as to melt and reflow the solder, and the soldered workpiece is then removed from the space containing the vapor.

In using the ether composition of this invention as a blowing agent in making plastic foam, such as foamed polyurethane, the process reactants, and reaction conditions described in U.S. Patent No. 5,210,106 (Dams et al.) can be used. In carrying out such process, organic polyisocyanate and high molecular weight compound with at least 2 reactive hydrogen atoms, such as a polyol, are admixed in the presence of a blowing agent mixture comprising an ether composition of this invention, catalyst, and a surfactant.

This invention is further illustrated by the following examples, but the particular materials and amounts thereof recited in these examples, as well as other conditions and details, should not be construed to unduly limit this invention.

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Example 1. Preparation of C_8F_{17} -O- C_2F_4H from C_8F_{17} -O- $C_2F_4CO_2CH_3$

The organic starting material, C_8H_{17} -O- $C_2H_4CO_2CH_3$, was prepared by base-catalyzed Michael addition of noctanol to acrylonitrile, followed by acid-catalyzed methanolysis. The methyl ester was directly fluorinated with F_2 to produce the fluorinated ester, C_8F_{17} -O- $C_2F_2CO_2CF_3$. This fluorination was carried out in a 2-liter, jacketed reactor vessel of Monel metal equipped with a magnetic drive agitator, gas feed line, organic reactant feed line, and a reflux condenser. The gas feed line was 0.3 cm diameter tube reaching to a point below the bottom impeller of the agitator. The feed line was a 0.15 cm diameter tube connected to a syringe pump. The reflux condenser consisted of about 6-meters of two coiled concentric tubes, the inner tube having a 1.27 cm diameter and the outer tube having a

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2.54 cm diameter. Gases from the reactor were cooled in the inner tube by refrigerant, ethylene glycolwater, flowing in the annulus between the two tubes. The reactor was charged with about 1.8 liters of Freon 113 chlorofluorocarbon and purged with 650 mL/min of nitrogen for 20 minutes. The gas stream was then changed to a mixture of 310 mL/min fluorine and 1100 mL/min nitrogen. After about 12 minutes, 100 g of C₂H₁₂-O-C₂H₄-CO₂CH₃, diluted to 260 mL with Freon^m 113 chlorofluorocarbon, was fed to the reactor at a rate of 13 mL/hr (5 g/hr feed rate). The reactor contents were maintained at about 16-18°C throughout the fluorination. The condenser temperature was about -22°C. The fluorine flow was continued for ten minutes after complete addition of the organic feed. reactor was then purged with nitrogen for one hour. The Freon™ 113 solution of the crude perfluorinated ester was treated with 150mL of 14% BF3 in methanol and agitated vigorously for 24 hrs. The mixture was washed with water, dried over MgSO4 and distilled (b.p. $40^{\circ}\text{C/O.2 torr}$ to yield $C_8F_{17}-O-C_2F_4-CO_2CH_3$ (47% yield). For purposes of decarboxylation, 39 g of 85% KOH was dissolved in approximately 300 mL of ethylene glycol and the above-described fluorinated methyl ester was added dropwise with stirring to the KOH solution at room temperature. Upon complete addition, the reaction mixture had a pH of 8 to 9. The mixture was heated slowly with stirring and the product of decarboxylation, C_8F_{17} -O- C_2F_4H , was distilled along with methanol from saponification of the methyl ester, water 30 from the KOH and a small amount of ethylene glycol. When the reaction mixture temperature reached 170°C, the heating was stopped. The lower fluorochemical phase of the distillate was separated, washed with water, dried and distilled through a three-plate Snyder column. The main fraction, boiling at 146-150°C, yielded 122 g of product. Gas chromatography and mass

spectrometry (GC/MS) of a sample of the product showed the sample to be 94% pure and confirmed the structure as C_8F_{17} -O- C_2F_2H .

Example 2. Preparation of C_8F_{17} -O- C_2F_4H from C_8F_{17} -O- $C_2F_4CO_2H$

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 C_8H_{17} -O- $C_2H_4CO_2CH_3$ was prepared by base-catalyzed Michael addition of n-octanol to acrylonitrile, followed by acid-catalyzed methanolysis. This carboxylic acid ester was directly fluorinated by essentially the same fluorination procedure described in Example 1 to produce the corresponding ether acid, C_8F_{17} -O- C_2F_4 COOH upon hydrolysis. Differential scanning calorimetry revealed multiple transitions, which is characteristic of polymorphism.

A solution of 116 g of 85% KOH in 800 mL of ethylene glycol was prepared in a 3 L round-bottom flask. 1000 g of the $C_8F_{17}OC_2F_4-CO_2H$ was added dropwise to the stirred KOH solution. Upon complete addition, an additional 10 g of KOH was added and the mixture heated. The fluorochemical product of decarboxylation was distilled together with a small amount of water from the neutralization of the acid. The lower fluorochemical phase of the distillate was separated, washed with salt water, dried over Na_2SO_4 and distilled as in Example 1 to yield 817 g of $C_8F_{17}-O-C_2F_4H$.

Example 3. Preparation of C_7F_{15} -O- C_2F_4H from C_7F_{15} -O- $C_2F_4CO_2CH_3$

 C_7H_{15} -O- $C_2H_4CO_2CH_3$ was prepared by base-catalyzed Michael addition of n-heptanol to acrylonitrile, followed by acid-catalyzed methanolysis. 550 g of the corresponding methyl ester, C_7F_{15} -O- $C_2F_4COOCH_3$, (prepared by essentially the same fluorination and methanolysis procedures of Example 1), was added dropwise to a solution of 166.6 g of KOH in approximately 880 mL of ethylene glycol. The

fluorochemical product was recovered essentially as in Example 1 to yield 440 g which was distilled through a six-plate Snyder column and the fraction boiling from 130 to 131°C was collected (340 g). This fraction was combined with 8.5 g of KMnO4 and approximately 350 g of acetone and heated to reflux. After four hours, an additional 5 g of KMnO4 was added and the resulting mixture was heated for an additional 3 hours. The mixture was filtered, the filter cake washed with acetone, and water was added to the filtrate causing a lower fluorochemical phase to form which was then washed with water, followed by conc. H2SO4, with water, and then filtered through silica. and 19F NMR confirmed the reaction product to have the desired structure, C7F15-0-C2F2H. Gas-liquid chromatography of a sample showed it to be 98.7% pure.

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Example 4. Preparation of C_6F_{13} -O- C_2F_4 -O- CF_2H from C_6F_{13} -O- C_2F_4 -OCF $_2$ CO $_2$ CH $_3$

The starting material, C_6H_{13} -O- C_2H_4 -O- C_2H_4 -O-COCH₃, was prepared by acetylation of hexyloxyethoxy ethanol with acetyl chloride. The acetate was then converted to C_6F_{13} -O- C_2F_4 -OCF $_2$ CO $_2$ CH $_3$ by essentially the same fluorination and methanolysis procedures of Example 1. 548 g of this fluorochemical was combined with 144.2 g of KOH in 600 g of ethylene glycol. The resulting mixture was heated, distilled and the product, C_6F_{13} -O- C_2F_4 -OCF $_2$ H, was recovered as in Example 1. Total yield was 433 g. The product was again distilled (b.p 131°C) through a 12-inch (30.5 cm) perforated-plate column at atmospheric pressure. The structure of the product was confirmed by 1 H and 19 F NMR as C_6F_{13} -O- C_2F_4 -OCF $_2$ H. GC/MS revealed a sample of it to be 99.6% pure.

Example 5. Preparation of C_8F_{17} -O-CF₂H from C_8F_{17} -O-CF₂-CO₂CH₃

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 $C_8H_{17}-O-C_2H_4-O-(CO)CF_3$ was prepared by acetylation of octyloxyethanol with trifluoroacetic anhydride. 100 g of the trifluoroacetate was directly fluorinated by essentially the same fluorination procedures of Example 1 and the fluorination product was quenched with a solution of BF₃ in methanol to yield crude $C_8F_{17}-O-CF_2-CO_2CH_3$, which was further purified by distillation, b. 92-97°C @20 torr.

A 58 g sample of the latter methyl ester was decarboxylated using 10.8 grams of KOH in ethylene glycol and the product, C_8F_{17} -O-CF₂H, was recovered as in Example 1. The structure of the product was confirmed by ¹⁹F NMR. GLC revealed the product to be 99.6% pure, b. 134-136°C.

Example 6. Preparation of $C_4F_9-0-C_2F_4H$ from $C_4F_9-0-C_2F_4-CO_2CH_3$

The methyl ester, $C_4H_9-O-C_2H_4-CO_2CH_3$, was prepared by base-catalyzed Michael addition of n-butanol to acrylonitrile, followed by acid-catalyzed methanolysis. The methyl ester was then converted to the corresponding fluorinated methyl ester, $C_4F_9-O-CF_2CF_2-CO_2CH_3$, by essentially the same fluorination and methanolysis procedures described in Example 1.

1160 g of the latter methyl ester was added dropwise with stirring to 3103 g of ethylene glycol and 129.5 g of NaOH. The product was distilled (b.p. 83°C) and treated with $KMnO_4/acetone$, and worked up as in Example 3. The structure of the purified compound, $C_4F_9-O-CF_2CF_2H$, was confirmed by 1H and ^{19}F NMR and GC/MS.

A sample of this compound was evaluated for use in precision cleaning applications by measuring the solubilities of selected hydrocarbon solvents in the sample. High solubility would indicate improved performance as a cleaning agent relative to perfluorocarbon solvents. The following hydrocarbon

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solvents were found to be soluble in amounts up to 50% by weight with the ether hydride: hexane, heptane, toluene, acetone, 2-butanone, 4-methyl-2-pentanone, ethyl acetate, methanol, ethanol, isopropanol, dimethyl formamide, trans-1,2-dichloroethylene and isopropyl ether. o-Xylene was found to be soluble to 19% by weight. Chloroform was found to be soluble to 45% by weight. Ethylene glycol was found to be soluble to less than 15% by weight and a light hydrocarbon oil was found to be soluble to less than 0.05% by weight.

A sample of the compound was also evaluated for use in spot-free drying applications such as taught in U.S. Patent No. 5,125,978 (Flynn et al.). A water displacement composition was prepared by dissolving 0.2% by weight of $C_4F_9OC_2F_4OCF_2CONHC_2H_4OH$ in $C_4F_9-O-C_2F_4H$. The solution was heated to $45^{\circ}C$ in an ultrasonic bath. Using the procedure described in U.S. Patent No. 5,125,978, test coupons of glass and stainless steel were wetted with water and subsequently immersed into this solution with ultrasonic agitation. All water was displaced within 60 seconds.

A sample of this compound was also evaluated for use as a rinse agent in co-solvent cleaning applications. (Such cleaning applications are taught, for example, in International Patent Publication No. WO 92/22678 (Petroferm Inc.). Organic esters such as methyl decanoate have found utility as solvating agents in two-phase cleaning applications using perfluorohexane as the carrier liquid and rinse agent.) Methyl decanoate and C4F9OC2F4H were placed in separate containers and heated to 50°C in an ultrasonic bath. 50 mm X 25 mm X 1.5 mm aluminum coupon was contaminated with 0.0831 g of a light hydrocarbon oil. contaminated coupon was first immersed in the methyl decanoate for about 60 seconds and then immersed in the $C_4F_9OC_2F_4H$ for about 60 seconds. The $C_4F_9OC_2F_4H$ rinsed 100 percent (as determined by weight difference) of the

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oil and the methyl decanoate from the coupon. Under the same conditions, perfluorohexane removed only 98.5 percent of the oil and methyl decanoate, indicating that $C_4F_9OC_2F_4H$ can be more effective as a carrier liquid and rinse agent than perfluorohexane.

Example 7. Preparation of $HCF_2CF_2-O-CF_2CF_2-O-CF_2CF_2H$ from $CH_3OC(0)C_2F_4-O-C_2F_4-O-C_2F_4C(0)OCH_3$

The starting material, $CH_3OC(0)C_2H_4-O-C_2H_4-O-C_2H_4-O-C_2H_4C(0)OCH_3$, was prepared by base-catalyzed Michael addition of ethylene glycol to acrylonitrile, followed by acid-catalyzed methanolysis. The starting material was then fluorinated and methanolysed by essentially the same procedures described in Example 1 to give $CH_3OC(0)C_2F_4-O-C_2F_4-O-C_2F_4C(0)OCH_3$.

1136 grams of the fluorinated ester was added to a mixture of 305.6 g of KOH in 2665 g of ethylene glycol. The decarboxylation was carried out essentially as described in Example 1, and the crude product distilled after phase separation but without water washing. The distillate still contained methanol which was removed by a wash with concentrated sulfuric acid followed by two water washes to give 695 g of the desired ether hydride product, with a boiling range of 93-94°C.

Example 8. Preparation of $C_4F_9-0-(CF_2)_5H$ from $C_4F_9-0-(CF_2)_5-CO_2H$

118.2 g (1.0 mol) hexane-1,6-diol, 4.4 g Adogen™
464 quaternary ammonium salt, 80.0 g (2.0 mol) NaOH,
and 250 mL tetrahydrofuran was stirred at reflux. 80
mL H₂O was added to get better mixing. After 20 min
more, 137 g (1.0 mol) butyl bromide was added over 0.5
hr, and stirred overnight at reflux. The reaction
mixture was quenched in 1 L H₂O, and the upper layer
was combined with an ether extract of the lower layer,
dried over MgSO₄, and stripped on a rotary evaporator.
Treating the resulting stripped layer (151 g) in 100 mL
CHCl₃ with 150 mL acetyl chloride added dropwise and

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subsequently heating at reflux 4 hr and solvent removal gave 225.4 g of liquid. Distillation of the liquid gave 176.0 g (b. 100-104°C/0.9 torr) of distillate. GLC indicated 56% of it to be the desired 6-butoxyhexyl acetate, accompanied by hexanediol diacetate and 5 dibutoxyhexane. 100 g of this mixture was fluorinated essentially as in Example 1. Treatment of the resulting fluorinated product with 30 mL of a 10 weight percent solution of H2SO4 in H2O and shaking at room temperature for 2 hours, filtration of solid 10 fluorinated adipic acid, separation of the F-113 layer, drying over MgSO4, and distillation produced a main cut of 73.4 g, b. 116°C/20 torr, 96% pure C_4F_9 -O-(CF_2)₅COOH. The latter was added to a solution of 10.0 g (0.25 mol) NaOH and 100 mL ethylene glycol and the mixture was 15 heated to 120°C, with $C_4F_9-O(CF_2)_6-O-C_4F_9$ impurity from fluorination collecting in the Dean-Stark trap. continued heating, gas evolution began and a liquid, $C_4F_9-O(CF_2)_5H$, (44.6 g) collected in the trap, ending by The collected liquid was dried over silica gel 20 and distilled on a 4-inch (10.2 cm) Vigreux column to 38.8 g, b.p 131°C. F-nmr confirmed structure, in high purity, to be C₄F₉-O-(CF₂)₅H.

25 Example 9. Preparation of C_5F_{11} -O- $(CF_2)_5H$ from C_5F_{11} -O- $(CF_2)_5COOH$

In a similar fashion to Example 8, hexanediol was alkylated with n-pentyl bromide, the product was acetylated, and the crude acetate, C_5H_{11} -O- (CH₂)₆OC(O)CH₃, was distilled (b. 125°C/3 torr) and the distillate was fluorinated essentially by the fluorination procedure of Example 1. The fluorinated ester was hydrolyzed to the corresponding acid.

Decarboxylation of the fluorinated acid, $C_5F_{11}O(CF_2)_5COOH$, with NaOH gave 829 g of product. The product was washed with water, dried over MgSO₄, and

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distilled to yield 555 g of C_5F_{11} -O- $(CF_2)_5H$, b. 145-149°C.

Example 10. Preparation of C_8F_{17} -O- $(CF_2)_5H$ from C_8F_{17} -O- $(CF_2)_5COOH$

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In a fashion similar to Example 8, hexanediol was alkylated with n-octyl bromide, the product was acetylated, and the resulting C_8H_{17} -O- $(CH_2)_6$ -O-COCH₃ was directly fluorinated and hydrolyzed as in Example 8 to C_8F_{17} -O- $(CF_2)_5$ COOH, which was recrystallized from perfluorohexane. The recrystallized acid (37.5 g) was mixed with 4.0 g NaOH and 100 mL ethylene glycol and heated to 185°C. The product was washed with water, and the residual 27.9 g was distilled to give pure C_8F_{17} -O- $(CF_2)_5H$, micro b.p. 195°C.

Example 11. Preparation of $C_4F_9-0-CF_2C(CF_3)_2CF_2H$ from $C_4F_9-0-CF_2C(CF_3)_2CF_2C1$

The alkylation of 2,2-dimethyl-1,3-propanediol with n-butyl bromide carried out essentially as in Example 8 gave the crude mono-alkylated product, which was treated with SOCl₂ to give C₄H₉-O-CH₂C(CH₃)₂CH₂Cl, b. 80-90°C/20-30 torr. This compound was then fluorinated as in Example 1 to give C4F9-O-CF2C(CF3)2CF2Cl. 20.0 g of the latter chloride was mixed with 5.3 g water-wet Raney Ni and 50 mL of NH3saturated methanol. The mixture was left shaking on a Parr hydrogenation apparatus for 3 days at about 25 °C, with most of the 21 kPa (3 psig) hydrogen pressure drop occurring in the first day. The product was recovered by filtration and quenched in water, yielding 7.9 g with some mechanical loss. 19F-nmr confirmed the A scaleup to 100 g product to be C₄F₉-O-CF₂C(CF₃)₂CF₂H. gave 47 g, distilled to b.p 135°C.

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Example 12. Preparation of $H(CF_2)_4-O-(CF_2)_4H$ from $Cl(CF_2)_4-O-(CF_2)_4Cl$

C1-(CH₂)₄-O-(CH₂)₄-Cl was fluorinated as in Example A mixture of 30.3 g 1 to provide $Cl(CF_2)_4=0-(CF_2)_4Cl$. $Cl(CF_2)_4-O-(CF_2)_4Cl$, 11.3 g fresh water-wet Raney Ni, and 200 mL methanol was purged for several minutes with $\mathrm{NH_{3}}$ and pressurized with 310 kPa (45 psig) hydrogen on a Parr hydrogenation apparatus at about 25 °C. hr, pressure had dropped to 255 kPa (37 psig) and the mixture had become acidic, with glass etching noted. More ammonia was added and the reduction was continued, dropping another 62 kPa (9 psig). The reaction product was filtered and quenched in water to give 15.4 g of lower phase, 68% pure product confirmed by GLC to be Distillation yielded 27.0 g, b. 121-H(CF2)4-0-(CF2)4H. 124°C, 87% pure.

Example 13. Preparation of $H(CF_2)_4-O-(CF_2)_4H$ and $Cl(CF_2)_4-O-(CF_2)_4H$ from $Cl(CF_2)_4-O-(CF_2)_4Cl$

A mixture of 50.0 g $Cl(CF_2)_4-O-(CF_2)_4Cl$ and 30 g Zn in butanol was stirred at $110\,^{\circ}C$ for 2 days. GLC of a sample of the resulting reaction product indicated partial conversion. 21 g more Zn was added and the mixture was heated one more day. Filtration and quenching of the resulting material in water gave 27.0 g of a colorless liquid. The product was 35% of $H(CF_2)_4-O-(CF_2)_4H$, 42% mono hydride, and 16% unreduced dichloride.

Example 14. Preparation of C_6F_{13} -O- CF_2CF_2H from C_6F_{13} -O- $C_2F_4CO_2H$

The starting material, $C_6H_{13}-O-C_2H_4-CO_2CH_3$, was prepared by the Michael addition of hexanol to acrylonitrile followed by acid-catalyzed esterification with methanol. The resulting ester was then fluorinated and hydrolyzed to give the $C_6F_{13}-O-C_2F_4CO_2H$.

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500 g of the acid C_6F_{13} -O- $C_2F_4CO_2H$, was added slowly to a solution of 68.7 g KOH in 700 g ethylene glycol. At the end of the addition, an additional 5 g of KOH was added to the homogeneous solution to bring the pH to 9. The decarboxylation was carried out as in Example 1 and subsequently distilled, producing 327 g of product, b. 104-107 °C. The product was treated with potassium permanganate essentially as in Example 3. GC/MS, ^{19}F nmr, ^{1}H nmr and IR confirmed structure of the product as C_6F_{13} -O- CF_2CF_2H .

Example 15. Preparation of C_6F_{13} -O-CF₂H from C_6F_{13} -O-CF₂CO₂CH₃

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The starting material, C_6H_{13} -O- C_2H_4 OC(O)CH₃, prepared by acetylation of ethylene glycol monohexyl ether, was fluorinated and decarboxylated by essentially the procedures of Example 1 to give 146 g of C_6F_{13} -O- CF_2H (b. 92-96°C).

Example 16. Preparation of CF₃CF(CF₃)CF₂-O-CF₂H from CF₃CF(CF₃)CF₂-O-CF₂CO₂CH₃

The starting material, $CH_3CH(CH_3)CH_2-O-CH_2CH_2-OC(0)CH_3$, was prepared by acetylation of ethylene glycol monoisobutyl ether and conversion by essentially the fluorination and methanolysis procedures of Example 1 to give the methyl ester, $CF_3CF(CF_3)CF_2-O-CF_2CO_2CH_3$, b. 118-120°C.

149 g of the methyl ester was added to 28.6 g of KOH in 700 g of ethylene glycol rapidly dropwise. The decarboxylation was carried out to afford, after distillation, the product cut, 70 g, b. 45-47°C, of 99% purity by GLC. The structure was confirmed by GC/MS, 1 H nmr, and 19 F nmr analysis as $CF_{3}-CF(CF_{3})CF_{2}-O-CF_{2}H$.

Example 17. Preparation of $C_4F_9-O-(CF_2)_4-O-(CF_2)_3H$ from $C_4F_9-O-(CF_2)_4-O-(CF_2)_3COOCH_3$

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The starting material, $C_4H_9-O-C_4H_8-O-(CH_2)_3CH_2OCOCH_3$, was directly fluorinated and methanolysed essentially by the procedures of Example 1 to produce $C_4F_9-O-C_4F_8-O-(CF_2)_3CO_2CH_3$. 56 g of the latter was added rapidly to a solution of 5.6 g KOH in 250 ml of ethylene glycol. The decarboxylation was carried out and the product phase separated, washed once with brine, and distilled to yield 36.6 g of product (b.p. 155-158°C) of GLC purity 100%. GC/MS, 1H , and ^{19}F nmr analysis confirmed the product to be $C_4F_9-O-(CF_2)_4-O-(CF_2)_3H$.

Example 18. Preparation of $(C_2F_5)_2CFCF_2-0-C_2F_4H$ from $(C_2F_5)_2CFCF_2-0-CF_2CF_2-C(0)OCH_3$

Starting material, $(C_2H_5)_2CHCH_2-O-CH_2CH_2C(O)OCH_3$, prepared by the Michael addition of 2-ethylbutanol to acrylonitrile followed by acid-catalyzed esterification with methanol, was fluorinated and methanolysed essentially by the procedures of Example 1 to give $(C_2F_5)_2CFCF_2-O-CF_2CF_2-C(O)OCH_3$, b.p. 159°C, the direct fluorination yield, based on the methyl ester starting material being 88%.

The decarboxylation was carried out essentially as in Example 1 and the product distilled at $108-110^{\circ}$ C to yield 145 g, the IR analysis of which was consistent with the structure $(C_2F_5)_2$ CFCF $_2$ -O-CF $_2$ CF $_2$ H.

Example 19. Preparation of $C-C_6F_{11}CF_2-O-C_2F_4H$ from $C-C_6F_{11}CF_2-O-C_2F_4C(O)OCH_3$

The starting material, $c-C_6H_{11}CH_2-O-C_2H_4C(O)OCH_3$, prepared by the reaction of cyclohexylmethanol with acrylonitrile followed by acid-catalyzed esterification with methanol, was then fluorinated and methanolysed with BF₃ in methanol by essentially the procedures of Example 1 to give a 65% yield (based on the fluorination) of $c-C_6F_{11}CF_2-O-C_2F_4C(O)OCH_3$.

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224 g of the latter fluorinated ester was added to a solution of 28.2 g of 85% KOH and 466 g ethylene glycol held at 60°C. The resulting mixture was then heated to 100°C and its pH adjusted to a pH greater than 7 by the addition of 5 g of 45 wt% aqueous KOH. Decarboxylation was carried out by distillation of the resulting mixture. The lower fluorochemical phase of the resulting distillate was separated therefrom, washed with an equal volume of water, and distilled at 123-126°C to give 155 g of a product (99.7% purity). The product was treated with KMnO4 in acetone to give $c-C_6F_{11}CF_2-O-C_2F_4H$.

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Example 20. Preparation of $C_4F_9-0-C_2F_4-0-C_3F_6H$ from $C_4F_9-0-C_2F_4-0-C_3F_6C(0)$ OCH₃

 $C_4H_9-O-C_2H_4-O-C_4H_8OC(O)CH_3$ was fluorinated and methanolysed by essentially the procedure of Example 1. The resulting product, $C_4F_9-O-C_2F_4-O-C_3F_6C(O)OCH_3$, in the amount of 419 g was rapidly added dropwise to a mixture of 49.4 g KOH in 800 g ethylene glycol. The resulting mixture was then heated slowly to a final flask temperature of 190°C. During such heating, methanol from the saponification of the ester, water, and

 $C_4F_9-O-C_2F_4-O-C_3F_6H$ distilled from the reaction mixture. Water was added to the distillate and the lower, fluorochemical phase (355 g) was separated and distilled (b. 120-122°C) to provide 308 g $C_4F_9-O-C_2F_4-OC_3F_6H$ (82% yield).

Example 21. Preparation of C_6F_{13} -O- C_4F_8 -H from C_6F_{13} -O- C_4F_8 -CO $_2$ CH $_3$

The starting material, C_6H_{13} -O- C_5H_{10} -OC(O)CH₃, was prepared by monoalkylation of 1,5-pentanediol with hexyl bromide, followed by acetylation with acetyl chloride. This compound was fluorinated and methanolysed by essentially the procedure of Example 1,

to give C_6F_{13} -O- C_4F_8 - CO_2CH_3 , b.p $100^{\circ}C$ @ 13 torr. This ester was decarboxylated by heating a solution of 200 grams of ester in 250 mL of ethylene glycol with 30 g of KOH until the hydride product distilled. This liquid was washed with water, dried over MgSO₄ to give 128 g of C_6F_{13} -O- C_4F_8 -H of 82% purity. This was further purified by distillation using a 12 plate packed glass column, b.p. $146^{\circ}C$. The structure was confirmed by ^{19}F NMR.

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Example 22. Preparation of C_6F_{13} -O- C_3F_6 -H from C_6F_{13} -O- C_3F_6 -CO₂-K⁺

The starting material, C_6H_{13} -O- C_4H_8 -OC(O)CH₃, was prepared by monoalkylation of 1,4-butanediol with hexyl bromide, followed by acetylation with acetic anhydride. This compound was fluorinated and methanolysed by essentially the procedure of Example 1, to give C_6F_{13} -O- C_3F_6 -CO₂CH₃. The methyl ester was saponified using excess KOH, and then dried in a vacuum oven to yield the potassium salt. 575 g of the salt was heated with stirring in 250 mL of ethylene glycol and the product hydride recovered from the distillate, b.p. 129°C. The structure was confirmed by ¹⁹F NMR.

Example 23. Preparation of C_5F_{11} -O- C_4F_8 -H from C_5F_{11} -O- C_4F_8 -CO₂-Na⁺

The starting material, C_5H_{11} -O- C_5H_{10} -O-C(O) CH_3 was prepared by monoalkylation of 1,5-pentanediol with pentyl bromide, followed by acetylation with acetyl chloride. This compound was fluorinated and methanolysed by essentially the procedure of Example 1, to give C_5F_{11} -O- C_4F_8 -CO₂CH₃. The methyl ester was saponified using excess NaOH, and decarboxylated and distilled essentially as in Example 22. Distillation through a twelve-plate packed glass column gave pure C_5F_{11} -O- C_4F_8 -H, b.p. 125°C. The structure was confirmed by ¹⁹F NMR.

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Example 24. Preparation of C_4F_9 -O- C_3F_6 -H from C_4F_9 -O- C_3F_6 -CO₂-Na⁺

The starting material, $C_4H_9-O-C_4H_8-OC(O)$ CH_3 , was prepared by monoalkylation of 1,4-butanediol with butyl bromide, followed by acetylation with acetyl chloride. This compound was fluorinated and methanolysed by essentially the procedure of Example 1, to give $C_4F_9-O-C_3F_6-CO_2CH_3$. This methyl ester was saponified, decarboxylated and the crude hydride recovered as in Example 23, and then further distilled to yield pure $C_4F_9-O-C_3F_6-H$, b.p. $90^{\circ}C$. The structure was confirmed by ^{19}F NMR.

Example 25. Evaluation of surfactant activity of perfluoroether carboxylic acids.

The surfactant activity of novel perfluoroether carboxylic acids of this invention was measured with a DeNucy tensiometer after conversion of the acids to the corresponding ammonium salts. The acids were prepared by direct fluorination of their hydrocarbon precursors, followed by hydrolysis. The ammonium salts were prepared by treatment of the acid with excess aqueous ammonia followed by freeze drying. The results are reported in dynes/cm in the following Table C which lists the parent acid (from Table B) of the ammonium salt.

TABLE C

Parent Acid	Melting Point(s) of Acid (°C)	Suri	ace Tensi	ion (dyne	s/cm)
from Table B		Concentration of Ammonium Salt			
	·	50 ppm	100 ppm	500 ppm	1000 ppm
18	-1	24	21	18	
2		21	24		
4		63	59	39	29
5		33	33	26	22
7	19	37	26	19	17

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Parent Acid	Melting	Surf	ace Tensi	on (dyne	s/cm)
from Table B	Point(s) of Acid (°C)	Concen	tration o	of Ammoni	um Salt
		50 ppm	100 ppm	500 ppm	1000 ppm
6		31	23	18	17
8		33	31	26	24
9		38	24	20	18
10		38	35	24	19
27	-39	67	63	50	43
29	-9	49	43	29	23
35		18	18	16	16
25	-9	19	15	15	14
30	·	46	43	32	24
31		69	68	48	52
32		63	54	31	21
33		28	21	15	
40		48	41	23	19
11	49,59	18	15	15	
14		39	31	18	
15	16,-27	30	17	17	
16		24	19	18	17
17	90	14	15	15	

Example 26. Evaluation of ethers as fire extinguishing agents.

Omega-hydrofluoroalkyl ether compounds of this invention were evaluated as fire extinguishing agents using the National Fire Protection Association 2001 Fire Protection Standard, with a cup burner modified to handle liquid compounds. The results, shown below in Table D, indicate that the compounds could be effective agents for fire extinguishing, explosion suppression, and as flammable atmosphere inerting agents.

TABLE D

Agent	Extinguishment concentration, vol. %
C ₄ F ₉ OC ₂ F ₄ H	5.6
HC ₃ F ₆ OC ₃ F ₆ H	5.7

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Example 27. Preparation of foamed polyurethane.

Omega-hydrofluoralkyl ether compounds of this invention were evaluated as blowing agents for foams using the procedures taught in U.S. Patent No. 5,210,106 (Dams et al.). Component A contained 15.0 parts by weight of PAPIT27, a methylene diphenyldiisocyanate having an isocyanate equivalent of 134.0, available from Dow Chemical. Component B of the foam contained 10.5 parts by weight (pbw) of Voranol 360, a polyether polyol with a hydroxyl number of 360 available from Dow Chemical; 0.26 pbw of water; 0.26 pbw of an oligomeric fluorochemical surfactant as described in Example 1 of U.S. Patent No. 3,787,351; 0.13 pbw of Polycat 8, a N,N-dimethylcyclohexylamine catalyst available from Air Products; and 1.87 pbw of C4F9OCF2CF2H as the blowing agent.

The ingredients of Component B were mixed to obtain an emulsion which was then admixed with Component A and stirred at 2500 rpm for 10 seconds. The cream time of the foam was approximately 10 seconds. Rise time and tack-free time was approximately 2 and 3 minutes respectively. The

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resulting polyurethane foam was rigid and had a uniform distribution of very fine, closed cells.

Example 28. Preparation of $(CF_3)_3COC_2F_4OCF_2OCF_2CO_2CH_3$. The precursor, $(t-C_4H_9OC_2H_4O)_2CH_2$, prepared by alkylation of methylene chloride with t-butoxy ethanol, was fluorinated and methanolysed essentially as in Example 1 to yield $(CF_3)_3COC_2F_4OCF_2OCF_2CO_2CH_3$, having a boiling range $80-82^{\circ}C$ at 18 torr, and whose structure was confirmed by ^{19}F NMR.

Example 29. Preparation of $C_8F_{17}OCF_2OC_3F_6H$ from $C_8F_{17}OCF_2OC_3F_6CO_2CH_3$.

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The precursor, $C_8H_{17}OCH_2OC_4H_8OH$ was prepared by monoalkylation of butane diol with octyl chloromethyl ether. The precursor was first acetylated with acetyl chloride in methylene chloride containing triethylamine and then fluorinated, and a portion of the crude perfluorinated product was hydrolyzed by treatment with aqueous sulfuric acid and then distilled to yield the carboxylic acid $C_8F_{17}OCF_2OC_3F_6CO_2H$, having a boiling range $100-106^{\circ}C$ at 1.1 torr. Differential scanning calorimetry revealed the acid had a T_g of $-97.0^{\circ}C$ and several crystalline exotherms of -77.4, -61.5 and $-37.7^{\circ}C$ and a broad melting point at $-9.0^{\circ}C$.

Another portion of the crude perfluorinated products was methanolysed essentially as in Example 1 to yield $C_8F_{17}OCF_2OC_3F_6CO_2CH_3$, having a boiling range 124-130°C at 25 torr. The latter methyl ester was then decarboxylated using the procedure of Example 1 to yield $C_8F_{17}OCF_2OC_3F_6H$, having a boiling range of 178-183°C; the structures of this hydride and the precursor fluorinated ester were confirmed by ¹⁹F NMR.

Example 30. Preparation of $C_8F_{17}O-(C_2F_4O)_2CF_2CO_2H$. The precursor was prepared by monoalkylation of triethylene glycol with octyl bromide, followed by

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acetylation. The precursor was fluorinated as in Example 1, hydrolyzed by treatment with aqueous sulfuric acid, and distilled, the product, $C_8F_{17}O-(C_2F_4O)_2CF_2CO_2H$, having a boiling range of $105-110\circ C$ at 1.4 torr, and a melting point of $24\circ C$.

Example 31. Preparation of $HC_3F_6OC_3F_6H$ from $CH_3O(CO)C_3F_6OC_3F_6COOCH_3$

- The starting diacetate, $CH_3C(0)OC_4H_8O-(C_4H_8O)_nC_4H_8OC(0)CH_3$, was prepared by acetylation of polytetramethylene glycol (average molecular weight of 250) with acetyl chloride. The diacetate was then converted to
- CH₃OC(O)C₃F₆O-(C₄F₈O)_nC₃F₆COOCH₃ by essentially the same fluorination and methanolysis procedures described in Example 1. 1400 g of the resulting mixture of diesters was distilled on a ten-plate glass-packed column to isolate $CH_3OC(O)C_3F_6OC_3F_6COOCH_3$.
- 278 g of the isolated fluorochemical was combined with 72 g of KOH in 250 mL of ethylene glycol. The resulting mixture was heated, distilled, and the product, $HC_3F_6OC_3F_6H$, was recovered essentially as in Example 1 (b.p. 84°C). The structure of the product was confirmed by ¹⁹F NMR.

Example 32. Preparation of n-C₁₂F₂₅OC₂F₄OC₂F₄OCF₂CO₂H.

The precursor, n-C₁₂H₂₅O(C₂H₄O)₃H, was prepared by monoalkylation of triethylene glycol with n-dodecyl bromide. After acetylation, the resulting product was fluorinated essentially as in Example 1, and the fluorinated product was concentrated and treated with 55.0 g NaOH in 300 mL water. After heating for 5 hours on a steam bath, the product was acidified with an excess of a 50 weight percent solution of H₂SO₄ in water and then extracted with FluorinertTM FC-75

perfluorinated liquid (a mixture of C_8 perfluorochemicals, b.p. 103°C) which had been heated to about 60°C on a steam bath. Distillation yielded pure $n-C_{12}F_{25}OC_2F_4OC_2F_4OCF_2CO_2H$ ($T_g=-62.7^{\circ}\text{C}$ and $T_m=69.2^{\circ}\text{C}$ by DSC).

Example 33. Preparation of

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The starting material, methyl 2-(3,4-dimethoxyphenyl) acetate was fluorinated essentially as in Example 1 to yield perfluoro-2-(3,4-dimethoxycyclohexyl) acetic acid after hydrolysis. This was then decarboxylated essentially as described in Example 1 to the perfluorinated ether hydride.

Example 34. Preparation of

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The starting material, methyl 3-(4-ethoxyphenyl)-trans-2-propenoate was prepared by condensation of 4-ethoxybenzaldehyde with malonic acid, followed by esterification. This methyl ester was fluorinated, methanolized, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride.

Example 35. Preparation of

The starting material was prepared by condensation of 2,2-diethyl propane diol with dimethyl 3-oxoglutarate. This dimethyl ester was fluorinated, methanolyzed to the diester, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether dihydride.

Example 36. Preparation of

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The starting material was prepared by reaction of 2,6-dimethylphenol with ethylene carbonate and subsequent acetylation with acetyl chloride. This acetate was fluorinated, methanolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride (b.p. 132°C).

Example 37. Preparation of

$$\underbrace{ \begin{array}{c} \text{CF}_{8} \\ \text{E} \\ \text{CF}_{8} \end{array}}_{\text{CF}_{8} \text{CF}_{2} \text{H}} \quad \text{from} \quad \underbrace{ \begin{array}{c} \text{CH}_{2} \text{CH}_$$

The starting material was prepared by the treatment of 2-(2,6-dimethylphenyloxy)ethanol (from Example 36) with thionyl chloride. This was fluorinated essentially as in Example 1, followed by Raney Ni reduction of the chloride essentially as described in Example 12 to produce the perfluorinated ether hydride.

Example 38. Preparation of

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The starting material was prepared from the addition of β-napthol to ethylene carbonate, followed by acetylation with acetyl chloride. This acetate was fluorinated, methanolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride (b.p. 171°C).

Example 39. Preparation of $C_5F_{11}OCF_2C(CF_3)_2CF_2H$ from $C_5H_{11}OCH_2C(CH_3)_2CH_2C1$

The starting material was prepared essentially as described above in Example 11. The ether chloride was fluorinated essentially as in Example 1, followed by Raney Ni reduction of the chloride essentially as described in Example 11 to produce the perfluorinated ether hydride (b.p. 148°C).

Example 40. Preparation of $(C_4F_9O)_2CFCF_2H$ from $(C_4H_9O)_2CHCH_2Cl$

The starting material was prepared by the addition of n-butanol to 2-chloroacetaldehyde and was fluorinated essentially as in Example 1, followed by Raney Ni reduction of the chloride essentially as

described in Example 11 to produce the perfluorinated ether hydride.

Example 41. Preparation of $CF_3O(CF_2)_9H$ from $CH_3O(CH_2)_{10}OAc$

The starting material was prepared by monoalkylation of 1,10-decanediol with dimethyl sulfate, followed by acetylation with acetyl chloride. This acetate was fluorinated, hydrolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride.

Example 42. Preparation of $C_9F_{19}OCF_2H$ from $C_9H_{19}OC_2H_4OAc$

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The starting material was prepared by monoalkylation of ethylene glycol with n-nonyl bromide, followed by acetylation with acetyl chloride. This acetate was fluorinated, hydrolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride (b.p. 155°C).

Example 43. Preparation of $(iso-C_3F_7)_2CFOC_2F_4H$ from $(iso-C_3H_7)_2CHOC_2H_4CO_2CH_3$

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The starting material was prepared by Michael addition of 2,4-dimethyl-3-pentanol to acrylonitrile, followed by methanolysis to the methyl ester. This ester was fluorinated, hydrolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride.

Example 44. Preparation of

The starting material was prepared by the alkylation of 4-ethylphenol with methyl chloroacetate. This ester was fluorinated, hydrolyzed, and decarboxylated essentially as in Example 1 to produce the perfluorinated ether hydride (b.p. 131°C).

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Example 45. Comparative Atmospheric Lifetimes and Boiling Points

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The atmospheric lifetime of various sample compounds was calculated by the technique described in Y. Tang, Atmospheric Fate of Various Fluorocarbons, M. S. Thesis, Massachusetts Institute of Technology (1993). As shown in the table below, the atmospheric lifetime of an ether hydride compound having two or more carbon atoms between the ether oxygen atom and the terminal hydrogen atom is considerably shorter than the atmospheric lifetimes of ether hydride compounds having only one carbon atom between the ether oxygen atom and the terminal hydrogen atom. Because of the shorter atmospheric lifetimes of the compounds of the present invention, these compounds are more environmentally acceptable.

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Compound	Atmospheric Lifetime
	(yrs)
C ₆ F ₁₃ OC ₂ F ₄ OCF ₂ H	>170
C4F9OC2F4OCF2H	>170
C _B F ₁₇ OCF ₂ CF ₂ H	80

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In addition, as shown in the table below, ether hydride compounds having two or more carbon atoms

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between the ether oxygen atom and the terminal hydrogen atom have lower boiling points than analogous non-ether compounds, and significantly lower boiling points than analogous ether hydride compounds having only one carbon atom between the ether oxygen atom and the terminal hydrogen atom. The unexpectedly low boiling points of compounds of the present invention render the compounds useful in processes involving temperaturesensitive substrates such as plastics. (For example, in vapor-phase cleaning, a substrate is rinsed in the condensing vapor of a boiling fluid, and in condensation heating, a substrate is heated by immersion in a boiling fluid.) In such applications, a lower-boiling fluid is preferred so as to avoid damage to the substrate. While it is known that boiling points can be reduced by selection of a compound having fewer carbon atoms, this may result in a boiling point reduction of 25°C or more, in addition to adversely affecting other properties such as solvency.

Compound	Boiling Point
	(°C)
C _B F ₁₇ CF ₂ H	136
C ₈ F ₁₇ OCF ₂ H	139
C ₇ F ₁₅ OC ₂ F ₄ H	131
F C ₃ F ₆ H	126
F C ₂ F ₄ OCF ₂ H	134
C ₂ F ₅ —F—OCF ₂ H	131
F CF2OC2F4H	125
C ₉ F ₁₉ CF ₂ H	154
C ₉ F ₁₉ OCF ₂ H	155
C ₈ F ₁₇ OC ₂ F ₄ H	148
C ₆ F ₁₃ OC ₄ F ₈ H	149
C ₅ F ₁₁ OC ₅ F ₁₀ H	150

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Various modifications and alterations of this invention will become apparent to those skilled in the art without departing from the scope and spirit of this invention.

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WHAT IS CLAIMED IS:

1. A normally liquid, omega-hydrofluoroalkyl sther compound represented by the general formula: $X-R_f-O(R_f'-O)_nR_f"-H$

wherein:

H is a primary hydrogen atom;

X is a fluorine atom, a primary hydrogen atom, or a primary chlorine atom;

n is an integer of 0 to 7; and

R_f, R_f', and R_f" are independently selected from the group consisting of linear or branched, unsubstituted perfluoroalkylene groups; linear or branched, perfluoroalkyl- or perfluorocycloalkyl-substituted perfluoroalkylene groups; and linear or branched perfluoroalkylene groups substituted with an ether oxygen-containing moiety;

with the proviso that when X is H or Cl, Rf has 1 to 18 chain carbon atoms, Rf' has 1 to 12 chain carbon atoms, and Rf" has 2 to 12 chain carbon atoms;

and with the further proviso that when X is F, then Rf has at least 4 chain carbon atoms, Rf' has 1 or more chain carbon atoms, and Rf" has 2 or more chain carbon atoms.

2. A normally liquid, omega-hydrofluoroalkyl 30 ether compound represented by the general formula:

$X-R_f-O+R_f'-O+_nR_f"-H$

wherein:

H is a primary hydrogen atom;

X is a fluorine atom, a primary hydrogen atom, or a primary chlorine atom;

n is an integer of 0 to 7; and

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R_f, R_f', and R_f" are independently selected from the group consisting of linear or branched, unsubstituted perfluoroalkylene groups; linear or branched, perfluoroalkyl— or perfluorocycloalkyl—substituted perfluoroalkylene groups; and linear or branched perfluoroalkylene groups substituted with an ether oxygen—containing moiety; with the proviso that when X is H or Cl, R_f has 1 to 18 chain carbon atoms and each of R_f' and R_f" independently has 1 to 12 chain carbon atoms; and with the further proviso that when X is F, then R_f has at least 4 chain carbon atoms, and each of R_f' and R_f" independently has 1 or more chain carbon atoms;

and with the still further proviso that when n is zero, then R_f is a perfluorocycloalkyl-substituted perfluoroalkylene group.

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- 3. A process for preparing an omegahydrofluoroalkyl ether compound of claim 1, which
 comprises decarboxylating the corresponding precursor
 fluoroalkyl ether carboxylic acid, hydrolyzable
 derivative of said carboxylic acid, or hydrolyzable
 precursor to said carboxylic acid or said derivative,
 said decarboxylating being carried out by contacting
 said precursor carboxylic acid or ester with a solution
 of inorganic base in protic solvent and heating the
 resulting reaction mixture.
- 4. A method of displacing water from a surface which comprises contacting the surface with a liquid composition comprising the omega-hydrofluoroalkyl ether compound of Claim 1.

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5. In a method of vapor phase soldering wherein a component to be soldered is immersed in or enveloped by a body of fluorinated liquid vapor to melt the solder, and the component is then withdrawn from the body of vapor, the improvement comprising using as the fluorinated liquid a composition comprising at least one omega-hydrofluoroalkyl ether compound of Claim 1.

6. A process for preparing a foamed plastic comprising the steps of:

admixing organic polyisocyanate and high molecular weight compound with at least 2 reactive hydrogen atoms in the presence of:

- blowing agent mixture comprising at least one omega-hydrofluoroalkyl ether compound of claim 1;
 - 2) a catalyst; and
 - 3) a surfactant.

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- 7. A method of removing a contaminant from an article comprising contacting said article with a composition comprising at least one omega-hydrofluoroalkylether compound of claim 1.
- 8. A method for the extinction of fires
 comprising applying to a fire a composition comprising
 at least one omega-hydrofluoroalkyl ether compound of
 claim 1.
- 9. A method for converting -CF₂Cl groups to -CF₂H groups comprising the step of contacting at least one compound containing at least one -CF₂Cl group with hydrogen gas, said contacting being carried out at a temperature below about 200°C in the presence of both a solution of base and a catalytic amount of at least one metal or supported metal, said metal being selected from the group consisting of nickel, palladium, and platinum.

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10. A compound represented by the formula: $R_{fg}=O-\left(CF_{2}\right)_{h}=Z$

where

R_{fs} is a linear or branched perfluoroalkyl group
having from 1 to 18 carbon atoms;

"b" is an integer of at least 3; and

Z is selected from the group consisting of -COOH, $-\text{COOM}_{1/v}$, -COONH₄, -COOR, -CH₂OH, -COF, -COCl,

-COR, -CONRR, -

 CH_2NH_2 , $-CH_2NCO$, -CN, $-CH_2OSO_2R$, -

CH2OCOR, -

CH2OCOCR=CH2,

-CONH(CH₂)_mSi(OR)₃,

and -

 $CH_2O(CH_2)_mSi(OR)_3$,

where M is an

ammonium

radical or a metal atom having a valence "v" of 1 to 4, each R is independently selected from the group consisting of alkyl groups having from 1 to 14 carbon atoms, fluoroalkyl groups having from 1 to 14 carbon atoms, aryl groups having from 6 to 10 ring-carbon atoms, and heteroatom-containing alkyl groups having from 1 to 14 carbon atoms, fluoroalkyl groups having from 1 to 14 carbon atoms, and aryl groups having from 6 to 10 ring-carbon atoms, and m is an integer of 1 to 11.

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11. A compound represented by the formula: $R_{\rm ft} - (O - R_{\rm ft}')_{\rm c} - O - (CF_2)_{\rm d} - Z$

wherein:

R_{ft} is a linear or branched perfluoroalkyl group having from 1 to 18 carbon atoms;

R_{ft}' is a linear or branched perfluoroalkylene group having from 1 to 11 carbon atoms;

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c is an integer of at least 1; d is an integer of at least 3; and Z is selected from the group consisting of -COOH, $-COOM_{1/v}$, $-COONH_4$, -COOR, $-CH_2OH$, -COF, -COCl, -COR, -CONRR, -CH2NH2, -CH2NCO, -CN, -CH₂OSO₂R, -CH₂OCOR, -CH₂OCOCR=CH₂, -CONH(CH₂)_mSi(OR)₃, and -CH₂O(CH₂)_mSi(OR)₃, where M is an ammonium radical or a metal atom having a valence "v" of 1 to 4, each R is independently selected from the group consisting of alkyl groups having from 1 to 14 carbon atoms, fluoroalkyl groups having from 1 to 14 carbon atoms, aryl groups having from 6 to 10 ring-carbon atoms, and heteroatom-containing alkyl groups having from 1 to 14 carbon atoms, fluoroalkyl groups having from 1 to 14 carbon atoms, and aryl groups having from 6 to 10 ring-carbon atoms, and m is an integer of 1 to 11.

Internation 1 Application No. PCT/US 95/06110

A. CLASSIPICATION OF SUBJECT MATTER
IPC 6 CC7C43/12 C07C59/135

B01D12/00

B23K35/38

C07C69/708 C08G18/08

C07C41/18 A62D1/00

CO7C41/24

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols) CO7C BO1D B23K CO8G A62D F26B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP,A,O 261 501 (HOECHST) 30 March 1988	1,2
X	JOURNAL OF FLUORINE CHEMISTRY, vol.10, no.1, July 1977, LAUSANNE CH pages 75 - 80 D. D. DENSON ET AL 'Synthesis of some perfluoroalkylether compounds'	1,2
X	JOURNAL OF HETEROCYCLIC CHEMISTRY, vol.10, no.6, December 1973, PROVO US pages 943 - 946 T. S. CROFT ET AL 'Fluoroalkyl-s-triazines' see paragraph bridging pages 944 and 945	1-3

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Special categories of cited documents: A document defining the general state of the art which is not considered to be of particular relevance E* carlier document but published on or after the international filing date L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) O* document referring to an oral disclosure, use, exhibition or other means P* document published prior to the international filing date but later than the priority date claimed	'T' later document published after the international filling date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention 'X' document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone 'Y' document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is considered to involve an inventive step when the documents, such combination heing obvious to a person skilled in the art. '&' document member of the same patent family
Date of the actual completion of the international acarch 14 September 1995	Date of mailing of the international search report 2 2 . 0 9 . 9 5
Name and mailing address of the ISA Fluropean Patent Office, P.B. 5818 Patentian 2 NL - 2280 HV (tipswijk Tel. (+ 31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+ 31-70) 340-3016	Authorized officer Wright, M

X Further documents are listed in the continuation of hox C.

Patent family members are listed in annex.

Internate 1 Application No PCT/US 95/06110

•		PC1/03 95/0	0110
C.(Cohunua	tion) DOCUMENTS CONSIDERED TO BE RELEVANT	10.	levant to claim No.
Calegory *	Citation of document, with indication, where appropriate, of the relevant passages	Ke	evant to train 140,
X	TETRAHEDRON LETTERS., vol.30, no.48, 1989, OXFORD GB pages 6717 - 6720 CHANG-MING HU ET AL 'Mechanistic study on the photooxidation of perhalofluoroalkyl sulfinates'		1,2
X	US,A,3 706 773 (L. G. ANELLO ET AL) 19 December 1972 see examples 7-10,12-14,16-18		10
X	US,A,3 674 800 (R. F. SWEENEY ET AL) 4 July 1972 see examples 1,5		10
X	US,A,3 766 274 (L. G. ANELLO ET AL) 16 October 1973 see examples 12,13		10
x	JOURNAL OF ORGANIC CHEMISTRY OF THE USSR., vol.15, no.7, July 1979, NEW YORK US pages 1264 - 1271 V. V. BERENBLIT ET AL 'Synthesis and some transformations of derivatives of perfluoroalkoxycarboxylic acids' see pages 1266 and 1268, compound nos.VII-X,XXXIII		10
A	FR,A,1 373 014 (E. I. DU PONT DE NEMOURS) 17 August 1964 see page 5, column 2; claims		5

Internation LApplication No. PCT/US 95/06110

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		BE-A-	714160	16-09-68
		BE-A-	714161	16-09-68
		BE-A-	714162	16-09-68
		DE-A-	1768286	28-10-71
		DE-A-	1768287	18-11-71
		DE-A-	1768288	18-11-71
		DE-A-	1770262	30-03-72
		FR-A-	1574801	18-07-69
		FR-A-	1578003	14-08-69
		FR-A-	1599703	20-07-70
		FR-A-	1580225	05-09-69
		GB-A-	1224771	10-03-71
		GB-A-	1224773	10-03-71
		GB-A-	1224772	10-03-71
	•	GB-A-	1224774	10-03-71
		NL-A-	6805860	28-10-68
		NL-A-	6805861	28-10-68
		NL-A-	6805862	28-10-68
		NL-A-	6805864	28-10-68
		US-A-	3514487	26-05-70
		US-A-	3577465	04-05-71
		US-A-	3647887	07-03-72
		US-A-	3697564	10-10-72
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US-A-3674800	04-07-72	DE-A-	2017399	15-10-70
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OD IT DIVVELT		GB-A-	1308794	07-03-73
FR-A-1373014	04~01-65	NONE	·- ·	

rational application No.

PCT/US 95/06110

Box I Observations where co	rtain claims were found unsearchable (Continuation of item 1 of first sheet)
This international search report ha	s not been established in respect of certain claims under Article 17(2)(2) for the following reasons:
1. Claims Nos.: because they relate to sub	ject matter not required to be searched by this Authority, namely:
Claim 9 : the se	us of the international application that do not comply with the prescribed requirements to such ful international search can be carried out, specifically: earch has been limited to the preparation of ethers 1: the documentary search has been limited to acids, salts and esters (Rule 33.3 PCT)
Claims Nos.: because they are dependen	it claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).
Box il Observations where uni	ty of invention is lacking (Continuation of item 2 of first sheet)
This International Searching Autho	rity found multiple inventions in this international application, as follows:
1. As all required additional searchable claims.	tearch fees were timely paid by the applicant, this international search report covers all
2. As all searchable plaims co of any additional fee.	ould be searches without effort justifying an additional fee, this Authority did not invite payment
3. As only some of the require covers only those claims for	red additional search fees were timely paid by the applicant, this international search report or which fees were paid, specifically claims Nos.:
4. No required additional season restricted to the invention	rch fees were timely paid by the applicant. Consequently, this international search report is first mentioned in the claims; it is covered by claims Nos.;
Remark on Protest	The additional search fees were accompanied by the applicant's protest. No protest accompanied the payment of additional search fees.

A Status Report on the Development of HFC Blowing Agent for Rigid Polyurethane Foams

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ABSTRACT

The field of blowing agents for rigid polyurethane foams has seen a great deal of upheaval in the recent years. Starting with a situation where CFC-11 was the only blowing agent in use, various alternatives have emerged, among which HCFC-141b has become the product of choice when high thermal and fire performance are to be achieved. It is however already time to think again about a new generation of blowing agents that would have no impact on the ozone layer.

This paper provides an update on the actions undertaken by Elf Atochem (leading supplier to the rigid polyurethane foam market with FORANE® 141b) to prepare the future by developing zero ODP/high performance alternatives.

This will include the presentation of our latest laboratory results regarding the evaluation of several liquid and gaseous HFCs as blowing agents in rigid polyurethane foams such as HFC-134a, HFC-245fa, HFC-365mfc, HFC-245eb, HFC-245ca, HFC-236ea. The results of the evaluation of HFC-365mfc and HFC-134a by foam producers or raw material suppliers in different applications will also be presented.

CURRENT REGULATIONS ON OZONE DEPLETING SUBSTANCES

The discovery in the 70–80's that some molecules could have a very severe effect on the ozone layer has prompted the international community to enact stringent regulations on their production and/or uses.

From its enactment in 1987 and through its subsequent reviews, the now well-known Montreal Protocol has been the regulatory arm chosen by the international community for the control of substances that deplete the ozone layer. This international agreement provides a phase-out schedule that will differ depending on the type of substance con-

sidered and the group the country belongs to ("developed countries" and "article 5 countries"). For the products used as blowing agents in polyurethane foams, according to the Montreal Protocol, the production of CFCs in developed countries was forbidden on 1/1/1996. The "article 5 countries" will have until 2010 to end their production. HCFCs have also been included and have an elimination schedule of 2020 (gradual reduction from 2004 to 2020) for the developed countries and 2040 for the article 5 countries (gradual reduction from 2016 to 2040).

Within the frame of this protocol, some countries, such as the United States and the European Union, have decided to take further steps towards the total phase-out of all ozone depleting substances. The United States has decided, for example, HCFC-141b will have to be phased-out in 2003. Meanwhile, the European Union has phased-out CFCs on 1/1/1995. It has further placed restrictions on the uses of the HCFCs, limiting them to non-emissive applications, such as rigid insulating foams. In the European Union, HCFCs will be eliminated in 2014. This last regulation can even lead to some unexpected results since in the European Union, using HCFCs for flexible or integral skin polyurethane foams is therefore forbidden, but the use of CFCs is not.

Figure 1 summarizes these regulations. It is necessary to keep the whole picture in mind to understand the current developments in the field of blowing agents for rigid polyure-thane foams.

HCFC-141b: A SUCCESSFUL BLOWING AGENT

Since CFCs (CFC-11 in the case of rigid polyurethane foams) have by far the greatest Ozone Depletion Potential (as shown in Figure 2), the most effective way to help restore the ozone layer is to stop using them as soon as possible.

In developed countries, the phase-out of CFC-11 was made possible by the availability of substitutes (HCFC-

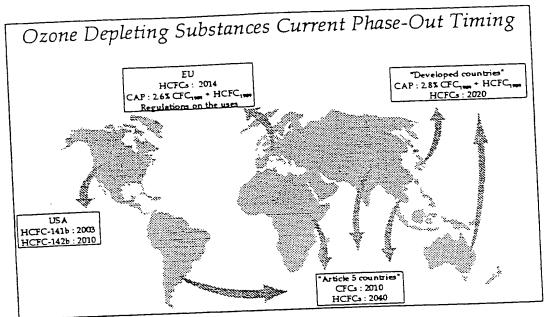


Figure 1.

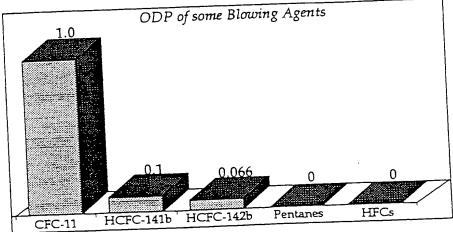


Figure 2.

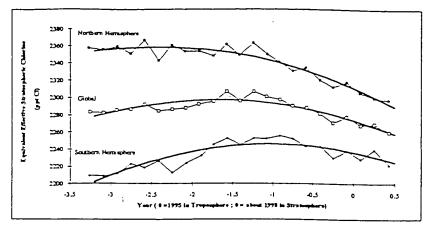


Figure 3.

141b in the US, HCFC-141b and hydrocarbons in the European Union). The phase-out of CFC-11 in foams, along with those made by the other application sectors (aerosols, refrigeration, fire extinguishers . . .), which were using ozone depleting substances, has already proven to be successful. The last measurements of the atmospheric chlorine loading [1] clearly show that we are on the right track. Indeed, as shown in Figure 3, the equivalent effective chlorine content in the northern troposphere (lower layer of the atmosphere) has been decreasing for a few years. Since chemical compounds in the troposphere need about 3 years to migrate to the stratosphere (upper layer of the atmosphere where the ozone layer is), we can expect to observe the same encouraging findings in the stratosphere before the end of the century; hence, the ozone layer should begin its recovery process very soon despite the fact that recovery will not be completed until several decades from now.

Therefore, the Montreal Protocol is already a success! Now, the most important issue is to help "article 5" countries to stop using CFCs as quick as possible. HCFCs, especially HCFC-141b, are the easiest and most efficient way to accomplish this goal.

There is concern that the European Union wants to expedite the total elimination of HCFC-141b. Such decision would not only have no meaningful effect on the recovery of the ozone layer, but also would send the wrong message to "article 5" countries: encourage them to continue using CFC-11 until 2010 rather than to switch to a possible threatened blowing agent like HCFC-141b or to hydrocarbons, with the large investments they require to be handled safely.

In spite of its small effect on the ozone layer, HCFC-141b has proven to be, and still is a necessary step towards the total elimination of CFC-11.

ZERO ODP GASEOUS BLOWING AGENTS

Even if HCFC-141b is still definitely necessary to the rigid polyurethane foam industry, the development of zero ODP substitutes has been ongoing for several years.

Among different candidates. HFCs have already appeared as the most promising candidates. They are efficient blowing agents, safe to handle and have a minimized overall impact on the environment [2]: zero Ozone Depletion Potential (ODP), low direct Global Warming Potential, very good energy efficiency and therefore a reduced indirect impact on the greenhouse effect (Total Equivalent

Warming Impact concept), very low Photochemical Ozone Creation Potential (the HFCs do not participate in the creation of atmospheric pollutant and therefore are not usually classified as Volatile Organic Compounds).

Among the HFCs, it is possible to distinguish between the gaseous and the liquid ones. Gases are not the preferred options for the expansion of polyurethane foams since they require specific handling procedures, pressure vessels, and may cause some frothing when used. However, since some gaseous HFCs are already available, they can be an appropriate answer for those who want to use immediately a zero ODP, non flammable blowing agent. HFC-134a, initially developed in refrigeration, is the first obvious choice to look at. Its main properties are summarized in Table 1.

As already reported elsewhere [3], the main drawback of HFC-134a is its limited solubility in most polyols for rigid polyurethane foams. To establish that aspect, its solubility has been determined experimentally in different polyols.

The polyols tested are listed in Table 2.

The experimental set-up is as follows:

- a known mass of the polyol, pure or blended, is introduced inside an aerosol can
- · a known amount of HFC-134a is then added
- the can is vigorously stirred for half an hour
- once the temperature of the can is stabilized at 25°C, the partial pressure of the blowing agent inside the can is measured

When applying this procedure, a plot of the blowing agent partial pressure versus the amount of HFC-134a solubilized inside the polyol can be obtained. Figure 4 displays the results obtained for four different polyols with

Table 1.

	HCFC-141b	HFC-134a
Formula	CH ₃ CFCl ₂	CF3CFH2
MW (g/mol)	117	102
B.P. (°C)	32.1	-26.4
d (g/cc) @20°C	1.24	1.22
λ _{gaz} @25°C (mW/mK)	9.7	13.5
Flash point	None	None
Flame lim. (% vot.)	5.8-17.7	None
ODP	0.10	0
GWP _{100v}	630	1300
Toxicity	Good	Good

		,	
·	•	Supplier	Polyether_Type
3750 3502	-, -	ARCO ARCO	Aromatic amine based Blend of polyethers: sorbitol based and glycerine based
3544 3528		ARCO ARCO	Sorbitol based Sorbitol based

HFC-134a. At a pressure of one bar, the amount of HFC-134a dissolved in polyols can be obtained; this data will indeed correspond roughly to the amount that it will be possible to incorporate in a polyol system and still keep the blend polyol/HFC-134a in a non pressurized container.

Except for the aromatic amine based polyether polyol (A3750), the amount of HFC-134a that can be solubilized in the other polyols, for a partial pressure of HFC-134a equal to one bar, is quite constant and is around 0.035 mole/100 g of polyol. This means therefore that around 3.5 parts of HFC-134a can be included in 100 parts of these polyols.

HFC-134a industrial scale trials have already been conducted in various locations throughout the European Union. Because of the limited solubility of HFC-134a in the standard polyols, most of the systems used so far included only low levels of HFC-134a (2-3 parts of HFC-134a in 100 parts of polyol) and were therefore largely water co-blown. Table 3 presents typical properties that can be achieved with this system.

As noted, results are quite satisfactory and could be improved by the use of higher HFC-134a levels perhaps by the direct injection of HFC-134a at the injection head.

ZERO ODP "LIQUID" BLOWING AGENTS— FOAMING TESTS

As we have shown earlier, HFC-134a can be a solution for those who want to use a non-flammable, zero ODP blowing agent immediately. There is, however still a need for a true "liquid" HFC substitute to HCFC-141b which will be able to replace it in all its applications. Several candidates have already emerged. A list of those candidates along with their principal physical properties is shown in Table 4. Among them are the three isomers of pentafluoropropane, HFC-365mfc, HFC-236ea and HFE-236 (which is in fact a commercially available molecule used as anaesthetic).

All these molecules were tested as blowing agents in the

same conditions. The formulations used are reported in Table 5. For comparison purposes, the same base polyol/catalyst/surfactant was used for the six HFCs and HCFC-141b was used as a baseline. Moreover, all the reactants were mixed at 5°C (hand made foams) in order to accommodate HFC-236ea, the blowing agent with the lowest boiling point in this set. An additional group of HCFC-141b foams was also made with all the chemical reactant kept at 20°C. This allows us to evaluate the influence of initial temperature.

Figures 5, 6 and 7 show the main characteristics of the foams obtained with the various systems.

From these results, the following trends can be outlined:

- The three pentafluoropropane isomers, namely HFC-245ca, HFC-245eb, HFC-245fa, yield good properties in all the areas surveyed: thermal conductivity (both initial and aged), compression set and open cell content.
- For this non-optimized formulation, HFC-365mfc stands just behind the previous blowing agents. Using a more suitable surfactant (see hereafter) would undoubtedly improve the results.
- On the other hand, the relatively low boiling point of HFC-236ea appears to play against this blowing agent since controlling the foam structure seems to be more difficult than with the other blowing agents (presence of holes and chimneys).
- Even if all the characteristics of HFE-236 seem to favour this compound as a blowing agent for rigid polyurethane foams (boiling point, gaseous phase thermal conductivity), the actual foaming tests reveal that its solubility in the polyurethane matrix is too high to have good foam performance.
- At last, the comparison of the polyurethane foams blown with HCFC-141b at 20°C and at 5°C shows that the later is close to the former except that the thermal conductivity is 1 mW/mK higher.

ZERO ODP "LIQUID" BLOWING AGENTS—COMPARATIVE DIFFUSION STUDY

Being able to assess the long term thermal properties of the polyurethane foams blown with these liquid HFCs is also a major issue in the substitution of HCFC-141b. One way to deal with this question is to observe the foam's thermal conductivity ageing. Such data have already been presented in Figure 5. Another possibility is to monitor the gas phase composition of a polyurethane foam to analyse how

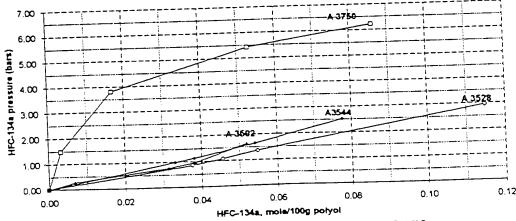


Figure 4. HFC-134a volatility vapor pressure of polyol mixtures @ 25°C

Table 3. Industrial trial for HFC-134a/H₂O systems in metal faced panels.

Thickness (mm)	70
Core density (g/l)	41.5
Compression set @ 10% (kPa)	140
Open cell content (%)*	2.3
Thermal conductivity @ 24°C (mW/mK)	
Initial	22.4
After ageing (7w @ rl + 9w @ 70°C)	23.1
Core cell gas composition: volume fractions Air/CO ₂ /HFC-134a	
initial	1.6/94.7/3.7
After ageing (7w @ n + 9w @ 70°C)	23.8/68.4/7.8
Dimensional stability (% vol. change)	
5d @ 90°C	-4.5
5d @ −18°C	-0.5

^{*}ASTM D 2856—Procedure B with an initial pressure step of 0.75 psi.

Table 4.

	HCFC-141b	HFC-236ea	HFC-365mfc	HFC-245ca	HFC-245eb	HFC-245fa	HFE-236
Formula	CH3CFCl2	CF₃CHFCF₂H	CF ₃ CH ₂ CF ₂ CH ₃	CFH ₂ CF ₂ CF ₂ H	CF₃CHFCH₂F	CF3CH2CF2H	CF3CHFOCF2H
MW (g/mol)	117	152	148	134	134	134	168
B.P. (°C)	32.1	6.5	40.0	25.4	22.7	15.3	22.8
d (g/cc) @20°C	1.24	1.40	1.25	1.40	1.38	1.32	1.45
λ _{gaz} @25°C (mW/m⋅K)	9.7	11.17	10.6*	10.8*	11.0*	11.2*	11.6*
Flash point	None	None	−25°C	None	None	None	None
Flame lim. (% vol.)	5.8-17.7	None	3.5-9.0	8.3-12.8	9.6-10.7	None	N.A.
ODP	0.10	0	0	0	0	0	0
HGWP	0.14	0.35	0.21	0.15	0.12	0.24	N.A.
Toxicity	Good	Pending	Pending	Pendina	Pendina	Pending	Good

^{*}Calculated data.

Table 5.

				Chemical Tem	perature (A/B)			
	20°C				5°C			
PU 1832 (BAYER system)	100	100	100	100	100	100	100	100
44v20 (iso index 105)	163	163	163	163	163	163	163	163
HCFC-141b	21	21						
HFC-245ca			24.4					
HFC-245eb				24.4				
HFC-2451a					24.4			
HFC-236ea						27.7		
HFC-365mtc							27	
HFE 236								30.€
Core density (g/l)	35.8	35 4	36.5	35.5	34.1	33.0	35.9	32.€

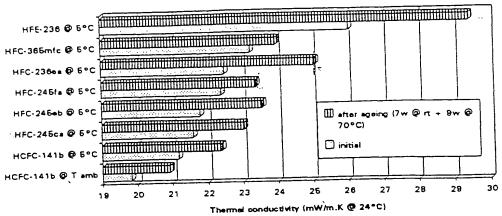


Figure 5. Blowing agent's effect on the thermal conductivity.

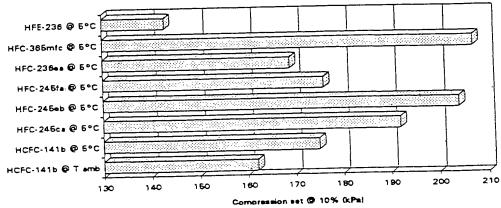


Figure 6. Blowing agent's effect on the compression set.

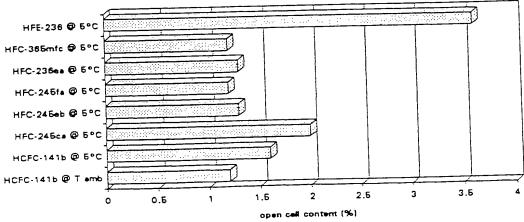


Figure 7. Blowing agent's effect on the open cell content. (ASTM D2856—Procedure B with an initial pressure step of 0.75 psi.)

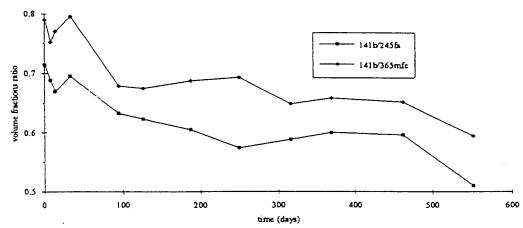


Figure 8. Comparative diffusion HCFC-141b/HFC-245fa/HFC-365mfc @ rt.

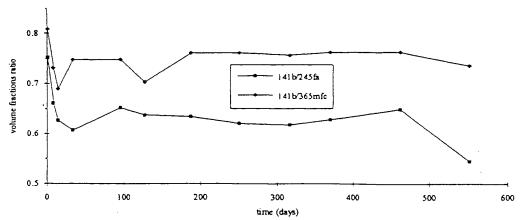


Figure 9. Comparative diffusion HCFC-141b/HFC-245fa/HFC-365mfc @ 70°C.

Table 6.

	Initial Volume Fractions (%)				
	Air	CO₂	HFC-245fa	HCFC-141b	HFC-365mfc
Sample 1 (to be aged @ rt)	1.5	38.5	22.4	16.8	20.8
Sample 2 (to be aged @ 70°C)	1.3	40.8	22.1	15.8	20.0

Table 7. Surfactants evaluation for HFC-365mfc based systems by OSI Specialties S.A.

Systems by co. c		
Polyol	100	
Isocyanate	175	
Water	1.8	
DMCHA	1.5	
Silicone	0.3 to 1.5	
HFC-365mfc	31	

Table 8. Surfactant evaluation for HFC-365mfc based systems by OSi Specialities S.A.

	HFC-365mfc Flowability* (cm/g)	HFC-365mfc Initial λ -value (mW/m-K @ 24°C)**	HCFC-141b (reference) Initial λ-value (mW/m·K @ 24°C)**
NIAX® L-6900 NIAX® L-6908 NIAX® SR- 321	0.95 0.93 0.72	22.7 23.0 23.1	- 22.1 21.7 /

Table 9. HFC-365mfc evaluation by Industrial Urethanes (system supplier—South Africa).

	(-)	
Poivol blend		79.8
Isocvanate (indi	ex 110)	128
Water	,	1.8
HFC-365mic		18.4
1 0 000		

Table 10. HFC-365mfc evaluation by Industrial Urethanes (system supplier—South Africa).

Cream time (hand mix)	15 seconds
String time	67 seconds
Tack free time	103 seconds
Free rise density	25.6 kg/m ³
Initial k-value @ 10°C	22.1 mW/mK
Compression strength 10%	247.4 kPa (parallel to rise)
Samples from Brett Mould (foam core density 31.8 kg/m³)	106.0 kPa (perpendicular to rise)
(loan core density 51.6 kg/m)	

^{*0.3} part of silicone
**1.5 part of silicone—Moulded foam; 34 g/i—tree rise density; 25.0 g/l.

fast these new blowing agents will leave the polyurethane foam (the long term thermal efficiency of a closed cell rigid polyurethane foam depends very much on the blowing agent diffusion out of the foam).

To that intent, a method has been developed to periodically analyse the content of the gas phase of a cellular polymer. The experimental set-up is relatively easy to implement: under a helium flow, a syringe needle is pushed inside the foam; then, the content of the broken cells is pulled into the syringe's body. Keeping the needle inside the helium stream, the content of the syringe is injected in a gas chromatogram and is analyzed for air, CO_2 and the various blowing agents. The helium flow is necessary in order to prevent any outside air from polluting the original cell content (which could happen since pressure within the cells might be below atmospheric pressure). With this method, it is thus possible to determine the volume fractions of all the components present in the gas phase of a foam. Moreover, since it is non destructive (only a few cells are broken for each determination), it is possible to follow the evolution of the cell gas composition with time.

The first step to study the comparative diffusion of some of the most likely substitutes has been to blow two polyurethane foams with a mixture HCFC-141b/HFC-245fa/HFC-365mfc. The initial cell gas contents analyzed according to the above procedure for the two polyurethane samples are

presented in Table 6.

Subsequent to this analysis, one sample has been aged at

room temperature and the other at 70°C.

In this case, we have followed the ratio of the volume fraction of HCFC-141b over HFC-245fa or over HFC-365mfc. Indeed, the volume fraction of HCFC-141b over the volume fraction of HFC-245fa is simply the ratio of the amount of HCFC-141b present in the gaseous phase over the amount of HFC-245fa in this same gaseous phase; the total volume, which would depend on the amount of air or CO₂, is no longer involved.

If we take a closer look at the amount of a physical blowing agent (HCFC-141b, HFC-245fa or HFC-365mfc) in the gaseous phase, it can only decrease through several mechanisms: diffusion of the blowing agent outside the foam, dissolution inside the polymer matrix or condensation within the cells. The only possibility to observe an increasing amount of blowing agent would have to come from a desorption from the matrix into the gas phase. Under usual circumstances, this is unlikely to happen.

So, for example, if the ratio of the volume fraction of HCFC-141b over HFC-245fa is increasing, it necessarily means that the amount of HFC-245fa in the gas phase has decreased faster than the amount of HCFC-141b. On the other hand, if this ratio has decreased, it necessarily means that the amount of HCFC-141b has decreased faster than

the amount of HFC-245fa.

Figure 8 represents the evolution of the ratio of the volume fractions of HCFC-141b over HFC-245fa and of HCFC-141b over HFC-365mfc for the polyurethane sample aged at room temperature. Figure 9 gives the same infor-

mation for the foam aged at 70°C.

Let's analyse first the evolution at room temperature. In both cases, the ratio of the volume fractions of HCFC-141b over HFC-245fa or over HFC-365mfc is clearly decreasing with time, meaning that HCFC-141b is disappearing faster from the foam's gas phase than HFC-245fa or HFC-365mfc. Therefore, we can expect a slower ageing (better aged there mal conductivity) for a polyurethane foam blown with either of these two HFCs than with HCFC-141b. As for the evolution at 70°C, the two ratios have again a marked de-

creasing trend at the beginning but a more constant aspect afterward. From this comparative diffusion study, we can say that long term thermal ageing of the foam should be at least as good with either HFC-245fa or HFC-365mfc as with HCFC-141b itself.

Our results show that efficient zero ODP substitutes for HCFC-141b do exist. Among them. HFC-245fa and HFC-365mfc appear to be the most promising when not only their performance as blowing agents for rigid polyurethane foams but also their ease of manufacture is considered. Moreover, HFC-365mfc has one more advantage over the other candidates since it can be a HCFC-141b substitute not only as a blowing agent but also as a solvent, which would expand its potential market, and therefore favourably impact its economics.

ZERO ODP "LIQUID" BLOWING AGENTS—HFC-365mfc CUSTOMERS' EVALUATIONS

All these facts have prompted Elf Atochem to pursue the evaluation of HFC-365mfc in collaboration with several PUR foam producers or raw material suppliers. As an example, OSi Specialties S.A. has been working on the identification of silicone surfactant especially suitable for HFC-365mfc based systems. Table 7 lists a typical laminated board formulation that was used by OSi Specialties.

Table 8 provides some of the results and shows that NIAX® L-6900 and L-6908 seem to give excellent performance with HFC-365mfc systems in terms of both foam flow-

ability and thermal conductivity.

Finally, HFC-365mfc has also been evaluated by Industrial Urethanes (system supplier—South Africa) in the formulation described in Table 9 and has yielded the results presented in Table 10.

These results are again very encouraging and clearly demonstrate the potential of HFC-365mfc as a blowing agent for rigid polyurethane foams.

CONCLUSION

Since many factors are necessary to qualify a candidate as an acceptable blowing agent (environmental impact, toxicity, flammability, foam performance) and since several other factors must be considered for a candidate to be selected as a commercial product (availability of feedstock, ease of manufacture, cost, market size), the objective for Elf Atochem is to be able to determine the best option within the next years, the following years being possibly dedicated to long term toxicological studies, pilot and plant construction and reformulation.

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